

# CO<sub>2</sub> Chemisorption and Cyclability Analyses of Lithium Aluminate Polymorphs ( $\alpha$ - and $\beta$ -Li<sub>5</sub>AlO<sub>4</sub>)

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**ABSTRACT:** The  $\alpha$ - and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> polymorphs were synthesized using a solid-state reaction. The polymorphs were then characterized by X-ray diffraction (XRD), X-ray thermodiffraction (XRTD), and N<sub>2</sub> adsorption. To determine the CO<sub>2</sub> chemisorption capacity, the lithium aluminate polymorphs were analyzed thermogravimetrically in the presence of a CO<sub>2</sub> flux. In addition, a cyclability study was performed on these ceramic materials. Although the results appear very similar for the two phases,  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> exhibits a better CO<sub>2</sub> chemisorption performance. The cyclic performance tests indicate that both materials exhibit a gradually reduced chemisorption capacity after multicycle processes. However, even after many cycles, the chemisorption capacity is considerably high in comparison to other lithium ceramics tested as CO<sub>2</sub> absorbents.

## 1. INTRODUCTION

Carbon dioxide (CO<sub>2</sub>) is a major anthropogenic greenhouse gas, which causes global warming and climate change. The rapid increase in Earth's population over the last few decades, combined with an improvement in the quality of life, are directly related to the dramatic increase in the concentration of man-made CO<sub>2</sub>, as both are related to the production and consumption of energy primarily obtained from fossil fuels.<sup>1–3</sup> To mitigate the impact of greenhouse gases, it is critical to trap CO<sub>2</sub> from fossil fuel power plants. The first step in carbon sequestration is the CO<sub>2</sub> capture from flue gas.<sup>3–6</sup> To this end, a variety of lithium ceramics have been tested as possible CO<sub>2</sub>-capturing materials.<sup>7–48</sup>

Among these ceramics, lithium aluminates (LiAlO<sub>2</sub> and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub>) were recently tested as possible CO<sub>2</sub>-capturing materials.<sup>49</sup> Although LiAlO<sub>2</sub> was unable to chemisorb CO<sub>2</sub>,  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> is able to capture CO<sub>2</sub> by a mechanism similar to the one reported for other lithium ceramics. Additionally, Li<sub>5</sub>AlO<sub>4</sub> appears to be one of the best options as a CO<sub>2</sub>-capturing material because of its high theoretical CO<sub>2</sub> chemisorption capacity due to its Li/Al molar ratio of 5 and the fact that aluminum is lighter than any other element tested, including zirconium, copper, and even silicon. The maximum CO<sub>2</sub> chemisorption capacity of  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> is 19.77 mmol/g, assuming that five lithium atoms react with CO<sub>2</sub> to produce Li<sub>2</sub>CO<sub>3</sub>. It should also be noted that  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> is able to chemisorb CO<sub>2</sub> over a wide range of temperatures (200–700 °C).<sup>49</sup> Therefore, because  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> has the best CO<sub>2</sub> chemisorption capacity per gram among various lithium ceramics, Li<sub>5</sub>AlO<sub>4</sub> is an important case of study as a CO<sub>2</sub> chemisorbent.

Two Li<sub>5</sub>AlO<sub>4</sub> polymorphs have been identified—the  $\alpha$ - and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub>—and detailed structural analyses have been performed.<sup>50,51</sup> The low temperature phase ( $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub>) transforms into a high temperature phase ( $\beta$ -Li<sub>5</sub>AlO<sub>4</sub>) at approximately 780 °C.<sup>52</sup> These structures are ordered

derivatives of the antifluorite (Li<sub>2</sub>O) structure with vacancies that occupy distinct lattice positions and can be formulated as Li<sub>5</sub>V<sub>2</sub>AlO<sub>4</sub>, where V represents a vacancy.<sup>53,54</sup> The  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase crystallizes in the orthorhombic space group *Pbca* with *a* = 9.087, *b* = 8.947, and *c* = 9.120 Å, with *Z* = 8. In contrast, the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase crystallizes in the orthorhombic space group *Pmmn* with *a* = 6.420, *b* = 6.302, and *c* = 4.620 Å, where *Z* = 2.<sup>50,51</sup> In both polymorphs, the metallic atoms (Li and Al) and the vacancies occupy tetrahedral sites and their ordered arrangement causes an orthorhombic distortion from cubic symmetry.

Therefore, the aim of this paper was to perform the synthesis and characterization of the  $\alpha$ - and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> polymorphs and then a kinetic analysis of the CO<sub>2</sub> chemisorption capacity and cyclability to determine if either of the two phases exhibit better CO<sub>2</sub> chemisorption behavior.

## 2. EXPERIMENTAL SECTION

The  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phases were synthesized using a solid-state reaction that employs lithium oxide (Li<sub>2</sub>O, Aldrich) and gamma aluminum oxide ( $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, Aldrich).<sup>55</sup> Initially, the powders were mechanically mixed and pressed into pellets (2.5 tons/cm<sup>2</sup>). Pellets must be used because the synthesis does not produce the desired product when powders are employed. Subsequently, the pellets were heated under different conditions: the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> pellets were heated to 500 °C for 24 h, while the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> pellets were heated to 900 °C for 24 h and rapidly cooled to room temperature. Finally, the  $\alpha$ - and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> pellets were pulverized. To obtain pure  $\alpha$ - and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub>, 30 and 20 wt % excess lithium was used, respectively, due to lithium's tendency to sublimate. The use of excess

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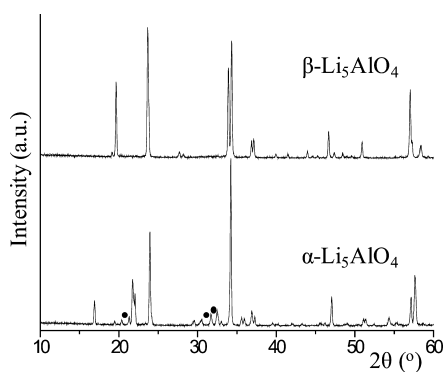
lithium in similar quantities than those mentioned above did not produce the corresponding pure phases.

Two different kinds of XRD measurements were performed: standard X-ray diffraction and X-ray thermodiffraction. In both cases, a diffractometer (Bruker AXS, D8 Advance) coupled to a copper anode X-ray tube was used. The  $\text{Li}_5\text{AlO}_4$  polymorphs were identified by the corresponding Joint Committee Powder Diffraction Standards (JCPDS). The X-ray thermodiffraction patterns were obtained by scanning from room temperature to 1000 °C, at a temperature step of 100 °C, using a platinum–rhodium holder. In this case, the thermal expansion of the X-ray thermodiffraction patterns was corrected using Pt peaks as the internal standard. Nitrogen adsorption–desorption isotherms and BET surface area analyses were performed using the Bel-Jpn. Minisorp II instrument at 77 K, using a multipoint technique. Samples were previously degassed at 85 °C for 12 h in vacuum.

Different thermal analyses were performed using a Q500HR instrument from TA Instruments. Initially, a set of samples was dynamically heated from room temperature to 900 at 5 °C/min, using a  $\text{CO}_2$  flow rate of 60 mL/min (Praxair, grade 3.0). Subsequently, the  $\text{Li}_5\text{AlO}_4$  samples were tested isothermally at different temperatures (from 350 to 675 °C) in the presence of the same  $\text{CO}_2$  flux. For the isothermal analysis, samples were initially heated to 675 at 100 °C/min with a subsequent isothermal treatment of 60 min, using a  $\text{N}_2$  flow. This procedure was conducted to ensure that all the samples received equivalent sintering prior to performing the  $\text{CO}_2$  chemisorption isotherms. Each sample was then cooled down to its respective isothermal temperature to perform an independent  $\text{CO}_2$  chemisorption process. Once the sample reached the corresponding temperature, the flow gas was switched from  $\text{N}_2$  to  $\text{CO}_2$  and the isothermal experiments were performed using a gas flow rate of 60 mL/min during the duration of the experiment. The regenerability tests were conducted under the uptake conditions in a  $\text{CO}_2$  atmosphere (700 °C for 20 min) and the desorption conditions in a  $\text{N}_2$  atmosphere (750 °C for 20 min). A flow rate of 60 mL/min was used for all gases. Finally, to elucidate the mechanism of  $\text{CO}_2$  capture by the  $\text{Li}_5\text{AlO}_4$  polymorphs, some of the products obtained from the thermal analyses were characterized by XRD.

### 3. RESULTS AND DISCUSSION

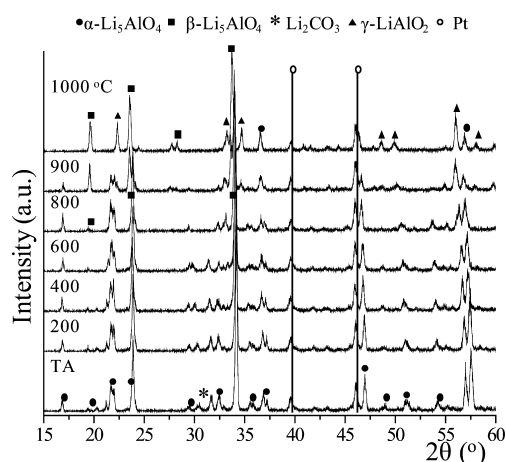
**3.1. Characterization.** Figure 1 presents the XRD patterns of the two lithium aluminate polymorphs. The low temperature



**Figure 1.** XRD patterns of both of the lithium aluminate polymorph samples. Peaks labeled with this symbol • correspond to  $\text{Li}_2\text{CO}_3$ .

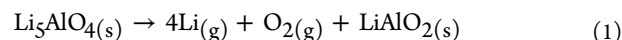
( $\alpha\text{-Li}_5\text{AlO}_4$ ) and the high temperature ( $\beta\text{-Li}_5\text{AlO}_4$ ) phases were synthesized using a solid-state reaction, and the data were fitted with the XRD patterns for 70–2643 and 70–0432 JCPDS files, respectively. Additionally, some small peaks corresponding to lithium carbonate ( $\text{Li}_2\text{CO}_3$ , JCPDS 22-1141) were found in the  $\alpha\text{-Li}_5\text{AlO}_4$  sample. The  $\text{Li}_2\text{CO}_3$  was not used as a reagent; thus, it must have been produced during the synthesis due to the use of excess lithium. It should be mentioned that similar amounts of  $\text{Li}_2\text{CO}_3$  were found in different iterations of  $\alpha\text{-Li}_5\text{AlO}_4$  synthesis, where the amount of excess lithium varied from 5 to 30% (data not shown). Therefore, it cannot be attributed to the excess lithium in the samples. In the case of  $\beta\text{-Li}_5\text{AlO}_4$ , there were no other phases detected by XRD, and thus, it could be considered a pure phase, at least according to the detection limit of XRD. Additionally, the surface area of both ceramics was measured using the BET model to be 0.5 and 0.2  $\text{m}^2/\text{g}$  for the  $\alpha$ - and  $\beta\text{-Li}_5\text{AlO}_4$  phases, respectively.

To check the thermal stability and transition temperature of the  $\alpha\text{-Li}_5\text{AlO}_4$  polymorph, a sample was analyzed by thermodiffraction (Figure 2). The XRD patterns did not



**Figure 2.** XRD patterns of the  $\alpha\text{-Li}_5\text{AlO}_4$  sample heated at different temperatures.

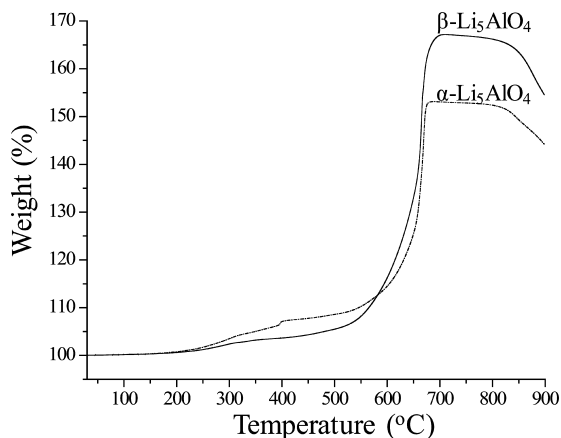
exhibit any changes between room temperature and 700 °C. However, when the sample was heated to 800 °C, the lithium carbonate peaks faded away because the melting point of  $\text{Li}_2\text{CO}_3$  is 720 °C. Additionally, the  $\beta\text{-Li}_5\text{AlO}_4$  phase began to appear. This result is in agreement with the  $\alpha$ - to  $\beta\text{-Li}_5\text{AlO}_4$  phase transition temperature, which is approximately 780 °C. Upon heating to 900 °C, the thermodiffraction pattern exhibited the formation of  $\gamma\text{-LiAlO}_2$  (JCPDS 38-1464). The  $\text{Li}_5\text{AlO}_4$  decomposed to form  $\gamma\text{-LiAlO}_2$ , which may have occurred via the sublimation of lithium, according to the following reaction 1:<sup>56</sup>



Lithium sublimation has been observed in several lithium ceramics in this temperature range (600–900 °C),<sup>9,57–60</sup> and in this case, the lithium sublimation must be accelerated as the thermodiffraction experiments were performed in a vacuum chamber. As a summary, the  $\alpha\text{-Li}_5\text{AlO}_4$  phase is stable until 700 °C because, above this temperature, the polymorphic transformation of  $\alpha$ - to  $\beta\text{-Li}_5\text{AlO}_4$  phase takes place.

**3.2.  $\text{CO}_2$  Chemisorption.** Once the samples were characterized and the thermal stability of the  $\alpha\text{-Li}_5\text{AlO}_4$  phase

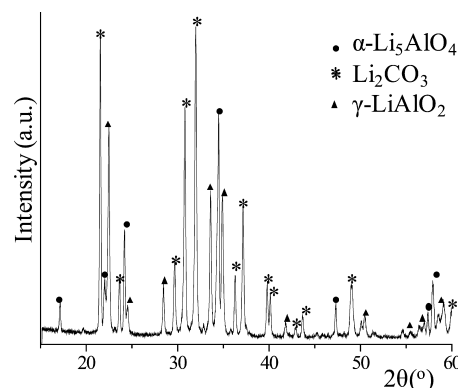
was evaluated, the CO<sub>2</sub> chemisorption capacities of both Li<sub>5</sub>AlO<sub>4</sub> polymorphs were analyzed thermogravimetrically in the presence of a CO<sub>2</sub> flux. Figure 3 provides the dynamic



**Figure 3.** Dynamic thermogram analysis of the both lithium aluminate polymorphs in a CO<sub>2</sub> flow.

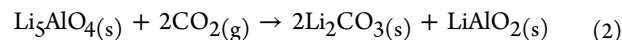
thermograms of  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> in the presence of a CO<sub>2</sub> flux. Both ceramics show similar trends and exhibit very high CO<sub>2</sub> chemisorptions, although via two different processes. The first increment of weight change occurred between 210 and 390 °C, and the second between 510 and 690 °C. These kinds of thermal trends have already been observed for other lithium ceramics.<sup>40,42,49,61,62</sup> For example, recently Li<sub>2</sub>CuO<sub>2</sub> was tested as a possible CO<sub>2</sub>-capturing material, and the results clearly showed that Li<sub>2</sub>CuO<sub>2</sub> is able to chemisorb CO<sub>2</sub> chemically in two similar steps.<sup>43</sup> First, at low temperatures, there is a CO<sub>2</sub> chemisorption over the surface of the ceramic, which suggests the formation of an external shell composed of alkaline carbonate. When the temperature is increased sufficiently, diffusion processes are activated, and the reaction continues through the bulk of the material, completing the CO<sub>2</sub> chemisorption. The diffusion processes indicate not only lithium diffusion but also oxygen diffusion because part of the oxygen present in lithium ceramics becomes part of the lithium carbonate external shell.<sup>75</sup> For the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub>, similar behaviors were observed. The surface reaction took place between 210 and 390 °C. The weight increments observed in this process were 5.42 and 2.88 wt % for the  $\alpha$ - and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub>, respectively. Subsequently, a weight increment of 6.4 wt % was observed between 390 and 580 °C for the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase, whereas the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase did not exhibit a change in weight. This behavior may be explained by the difference in the surface areas between the two polymorphs, which are 0.5 m<sup>2</sup>/g for the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> and 0.2 m<sup>2</sup>/g for the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub>. The surface area is an important factor at low temperatures, where the superficial CO<sub>2</sub> chemisorption takes place. At temperatures equal or greater than 510 °C, the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> absorbed 53.14% and 67.21% of CO<sub>2</sub>, respectively. At this temperature, the lithium diffusion should be activated, and the CO<sub>2</sub> chemisorption process was completed. Finally, at temperatures greater than 680 °C, the samples exhibited a desorption process. Although these results suggest that the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase chemisorbs more CO<sub>2</sub> than the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub>, this was only a qualitative analysis. A quantitative study was performed, and the results are described below.

To corroborate the reaction mechanism, the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> sample obtained after the CO<sub>2</sub> chemisorption process (at 700 °C) was characterized by XRD (Figure 4). As it can be seen in



**Figure 4.** XRD pattern of the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> sample after the CO<sub>2</sub> chemisorption process.

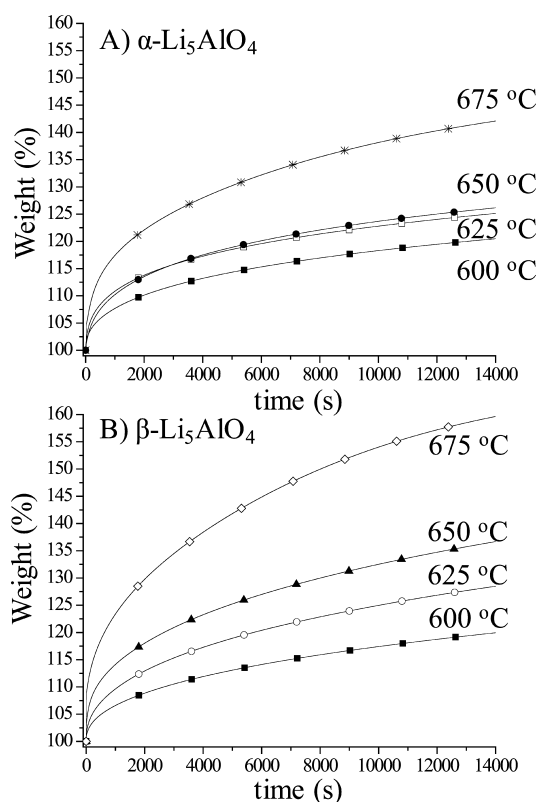
Figure 4, the XRD pattern was fit with the following JCPDS files: Li<sub>2</sub>CO<sub>3</sub> (22-1141),  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> (24-0596), and  $\gamma$ -LiAlO<sub>2</sub> (73-1338). These results confirm that the CO<sub>2</sub> is reacting chemically, producing Li<sub>2</sub>CO<sub>3</sub> and LiAlO<sub>2</sub> as products, independent of the initial phase Li<sub>5</sub>AlO<sub>4</sub>. Therefore, the correct reaction mechanism between Li<sub>5</sub>AlO<sub>4</sub> and CO<sub>2</sub> corresponds to the following reaction 2:



For this reaction, the actual Li<sub>5</sub>AlO<sub>4</sub> maximum CO<sub>2</sub> chemisorption capacity corresponds to 15.91 mmol/g. This result is in good agreement with the reaction system described by Inoue et al.,<sup>63</sup> which was derived from the phase diagram of the Li<sub>2</sub>O–Al<sub>2</sub>O<sub>3</sub> system.<sup>52</sup>

To further analyze the CO<sub>2</sub> chemisorption in the lithium aluminate polymorphs, different and independent kinetic experiments were performed. However, to eliminate the presence of any sintering effect, all the isotherms were initially heated to 675 at 100 °C/min with a subsequent isothermal treatment of 60 min using an N<sub>2</sub> flow. This procedure was performed to ensure that all samples were sintered in an equivalent manner prior to performing the CO<sub>2</sub> absorption isotherms, eliminating any sintering effect observed in previous works.<sup>49</sup> Each sample was then cooled down to its respective isothermal temperature for the CO<sub>2</sub> chemisorption. Once the sample reached the corresponding temperature, the flow gas was switched from N<sub>2</sub> to CO<sub>2</sub> and the isothermal experiments were performed. The kinetic data was only obtained for the initial CO<sub>2</sub> absorption, to avoid any kind of physical or chemical interference produced on the samples during the cycle processes.

As expected, all of the isothermal experiments followed a typical behavior (Figure 5), wherein the CO<sub>2</sub> chemisorption by both polymorphs increased as a function of temperature in an exponential manner. For the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase (Figure 5A), while the sample that was heated to 600 °C chemisorbed 20.3 wt % of CO<sub>2</sub> after 3.5 h, the total weight increment observed at 675 °C was 41.8 wt % for the same period of time. This means that at 675 °C, the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase is able to chemisorb twice as much CO<sub>2</sub> than at 600 °C. However, the samples heated between 625 and 650 °C increased their weight by only 25 and 26 wt %, respectively. In contrast, the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase (Figure



**Figure 5.** Isotherms of CO<sub>2</sub> chemisorption on both lithium aluminate polymorphs at different temperatures after a sintering process at 675 °C.

5B) showed that the amount of CO<sub>2</sub> chemisorbed increased dramatically as a function of temperature. Therefore, in the isothermal analyses at 600, 625, 650, and 675 °C, the weight gain was 20.2, 29.3, 37.4, and 59.4 wt %, respectively. This indicates that at 675 °C, the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase is able to chemisorb three times more CO<sub>2</sub> than at 600 °C. None of the isothermal analyses reached the plateau. The diffusion processes at this temperature appears to be slow for this polymorph. However, at 675 °C, the diffusion process is completely activated, and the surface area is not a critical factor. Additionally, at longer times, the maximum CO<sub>2</sub> chemisorption capacity increased in both polymorphs because at longer periods, the weight increment depends on the diffusion processes, which are activated at higher temperatures.

After the qualitative analysis of the isothermal experiments, the curves were fit to a double exponential model (eq 3) because it has been reported that two different processes take

place: CO<sub>2</sub> chemisorption over the Li<sub>5</sub>AlO<sub>4</sub> surface of the particles (*process 1*), which indicates the formation of an external shell of alkaline carbonate, and the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes (*process 2*).<sup>49</sup> The double exponential model to which the isotherms were fit is defined by the following equation:

$$y = A\exp^{-k_1t} + B\exp^{-k_2t} + C \quad (3)$$

where  $y$  represents the weight percentage of CO<sub>2</sub> chemisorbed,  $t$  is the time, and  $k_1$  and  $k_2$  are the exponential constants for the CO<sub>2</sub> chemisorption over the surface of the Li<sub>5</sub>AlO<sub>4</sub> particles and the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes, respectively. Additionally, the pre-exponential factors  $A$  and  $B$  indicate the intervals during which each process controls the whole CO<sub>2</sub> capture process, and the  $C$  constant indicates the  $y$ -intercept. The kinetics parameters, pre-exponential constants and  $R^2$  values obtained at each temperature are presented in Table 1.

These results demonstrate that the direct CO<sub>2</sub> chemisorption constant values ( $k_1$ ) are at least one order of magnitude higher than the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes constant values ( $k_2$ ). Additionally, the value of the  $B$  constants is always greater than that of the  $A$  constants. This means that the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes occurs during a larger interval of time than the CO<sub>2</sub> chemisorption produced directly over the surface of the particles. This behavior is explained by the fact that the CO<sub>2</sub> chemisorption occurs initially over the surface of the particles, but the majority of the Li<sub>5</sub>AlO<sub>4</sub> content is in the bulk of the ceramic, which necessitates the diffusion process. Finally, the constant values  $k_1$  were not very different for the  $\alpha$ - and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> polymorphs. However, the constant values  $k_2$  for the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase were lower by at least one order of magnitude than the constant values  $k_2$  for the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase, which indicates that the diffusion processes are more limited in the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase. Finally, all these results indicate that the rate-limiting step in the total process is the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes.

To quantitatively analyze these results and the temperature dependence of the different processes, the  $k_1$  and  $k_2$  constant values were fit to Eyring's model (eq 4), which is typically used on heterogeneous reactions and is a solid-gas system reaction in this case:

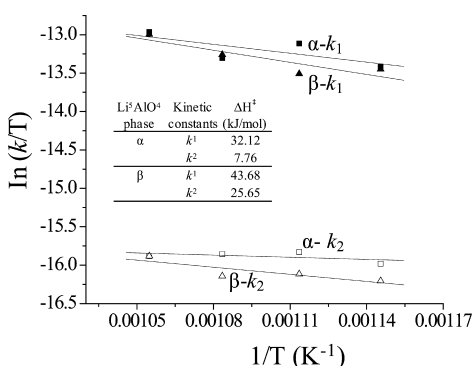
$$\ln(k_i/T) = -(\Delta H_i^\ddagger/R)(1/T) + \ln E + \Delta S_i^\ddagger/R \quad (4)$$

$k_i$  is the rate constant value of the process  $i$ ;  $E$  is the pre-exponential factor, which in Eyring's formulation is equal to the ratio between the Boltzmann and Planck constants;  $R$  is the

**Table 1.** Kinetic Parameters of the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> Isotherms Fitted to a Double Exponential Model

$T$ (°C)	$A$	$B$	$C$		$k_1$ (1/s <sup>-1</sup> )	$k_2$ (s <sup>-1</sup> )	$R^2$
				$\alpha$			
600	-5.226	-17.120	124.6		$1.30 \times 10^{-3}$	$1.00 \times 10^{-4}$	0.99955
625	-7.796	-18.284	128.6		$1.81 \times 10^{-3}$	$1.20 \times 10^{-4}$	0.99879
650	-7.949	-20.065	129.8		$1.54 \times 10^{-3}$	$1.20 \times 10^{-4}$	0.99949
675	-11.364	-32.781	148.0		$2.22 \times 10^{-3}$	$1.20 \times 10^{-4}$	0.99943
				$\beta$			
600	-4.368	-19.773	126.0		$1.26 \times 10^{-3}$	$8.00 \times 10^{-5}$	0.99967
625	-6.541	-27.382	136.7		$1.22 \times 10^{-3}$	$9.00 \times 10^{-5}$	0.99966
650	-8.090	-32.216	145.2		$1.61 \times 10^{-3}$	$9.00 \times 10^{-5}$	0.99936
675	-10.255	-49.258	168.4		$2.15 \times 10^{-3}$	$1.20 \times 10^{-4}$	0.99969

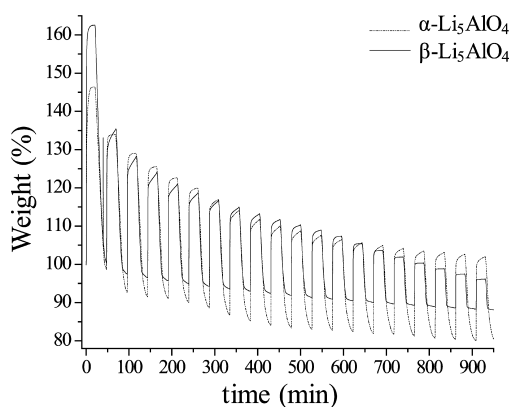
ideal gas constant; and  $\Delta H^\ddagger$  and  $\Delta S^\ddagger$  are the activation enthalpy and entropy, respectively. The data demonstrate that  $\ln(k/T)$  versus  $1/T$  plots can be described by a linear trend when using Eyring's model (Figure 6). Therefore, by fitting the



**Figure 6.** Eyring's plots for the rate constants values of the CO<sub>2</sub> direct chemisorption ( $k_1$ ), and the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes ( $k_2$ ).

data to a linear model, the activation enthalpies ( $\Delta H^\ddagger$ ) for the two different processes were calculated (see inset table of Figure 6). The  $\Delta H^\ddagger$  values obtained for the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase were 32.12 kJ/mol for direct CO<sub>2</sub> chemisorption and 7.76 kJ/mol for CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes. For the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> polymorph, the  $\Delta H^\ddagger$  values obtained were 43.68 and 25.65 kJ/mol for the direct CO<sub>2</sub> chemisorption and the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes, respectively. These results confirm that in both polymorphs, the CO<sub>2</sub> direct chemisorption process is more dependent on the temperature than the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes, at least in the temperature range of 600–675 °C. In other words, while the CO<sub>2</sub> direct chemisorption is considerably improved as a function of the temperature, the CO<sub>2</sub> chemisorption controlled by diffusion processes does not change significantly, which is inline with the  $k_2$  constant values reported in Table 1. In a previous paper,<sup>49</sup> the  $\Delta H^\ddagger$  values obtained indicated that the CO<sub>2</sub> chemisorption controlled by diffusion processes was more dependent on the temperature than CO<sub>2</sub> direct chemisorption. However, in that case, the  $\Delta H^\ddagger$  values were calculated from a considerably larger temperature range (300–675 °C). Nevertheless, the  $k_2$  constant values were varied by two orders of magnitude between 300 and 675 °C, but the values obtained, between 600 and 675 °C, are very similar to those obtained in this work. Therefore, the variations observed between these works must correspond to the temperature range taken into account in each case, wherein the  $\Delta H^\ddagger$  calculation is very sensitive to this parameter.

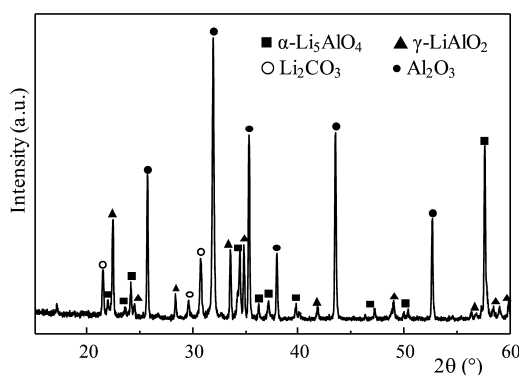
**3.3. CO<sub>2</sub> Cyclability.** To assess the regeneration properties and the thermal stability after several cycles of CO<sub>2</sub> chemisorption/desorption in both lithium aluminate polymorphs, the samples were tested using a multicycle method. Figure 7 shows the CO<sub>2</sub> chemisorption/desorption multicycle performance of the  $\alpha$ - and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> polymorphs. The result for the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase (dotted line) indicates that the CO<sub>2</sub> chemisorption capacity reaches approximately 47.7 wt % for the first cycle, and after 20 cycles, the CO<sub>2</sub> chemisorption capacity decreases to 22.1 wt %. For the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase (solid line), the CO<sub>2</sub> chemisorption in the first cycle was 62.3 wt %, but after 20 cycles, its capacity decreased dramatically to only 8.1 wt



**Figure 7.** Multicycle performance of CO<sub>2</sub> chemisorption/desorption on both lithium aluminate polymorphs. CO<sub>2</sub> absorptions were performed at 700 °C for 20 min, while the desorption processes were performed at 750 °C over 20 min into a N<sub>2</sub> flux.

%. Both polymorphs showed a similar behavior during the performance of several cycles. The CO<sub>2</sub> chemisorption decreased gradually after each cycle, and the achieved chemisorption capacity for the corresponding cycle subsequently reduced. The reduced capacity during the multicycle process may be caused by the following: as it can be seen in Figure 7, a fraction of the weight of the adsorbent is lost during the multicycle process, perhaps by the sublimation of Li<sub>2</sub>O during the desorption process, resulting in a reduction in the CO<sub>2</sub> chemisorption capacity. The  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase showed a higher Li<sub>2</sub>O sublimation of the two polymorphs because this phase is known to be stable at low temperatures. In contrast, the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase can exist at high temperatures. Additionally, we note that the CO<sub>2</sub> capture capacity in the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase is higher than that of the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase.

To understand the cyclability and the regeneration processes in the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase, a sample obtained after one CO<sub>2</sub> chemisorption/desorption cycle was characterized by XRD (Figure 8). The  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phases could be identified in the



**Figure 8.** XRD pattern of the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> sample after the CO<sub>2</sub> cyclic chemisorption process.

XRD patterns, as well as the Li<sub>2</sub>CO<sub>3</sub>,  $\gamma$ -LiAlO<sub>2</sub>, and Al<sub>2</sub>O<sub>3</sub> phases. These data indicate that the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> did not exhibit any phase transformation during the cycling experiments. The presence of Al<sub>2</sub>O<sub>3</sub> must be attributed to the diffraction generated by the support. Additionally, lithium carbonate cannot correspond to the compound produced during carbonation, as the desorption took place in N<sub>2</sub>, which indicates that the ceramic highly reacts with the environmental

Table 2. CO<sub>2</sub> Cyclic Results Obtained on Different Lithium Ceramic

sample	chemisorption temperature (°C)	desorption temperature (°C)	number of cycles	first CO <sub>2</sub> absorption (mmol/g)	last CO <sub>2</sub> absorption (mmol/g)	ref
Li <sub>4</sub> SiO <sub>4</sub>	700	850	5	2.5	2.5	70
Li <sub>4</sub> SiO <sub>4</sub>	600	800	50	1.93	1.65	64
Li <sub>4</sub> SiO <sub>4</sub>	650	750	5	1.91	2.1	33
Li <sub>4</sub> SiO <sub>4</sub> (dry milled sample)	740	820	6	2.5	2.5	21
Li <sub>4</sub> SiO <sub>4</sub> (wet milled sample)	740	820	10	2.08	1.25	21
Li <sub>4</sub> SiO <sub>4</sub> + 2 wt % Li <sub>2</sub> ZrO <sub>3</sub>	600	800	50	1.98	1.77	64
Li <sub>4</sub> SiO <sub>4</sub> + 5 wt % Li <sub>2</sub> ZrO <sub>3</sub>	600	800	50	2.28	2.14	64
Li <sub>3.7</sub> Fe <sub>0.1</sub> SiO <sub>4</sub>	650	750	5	1.91	1.16	33
Li <sub>4</sub> SiO <sub>4</sub> + 20 mol % K <sub>2</sub> CO <sub>3</sub>	600	600	10	4.54	4.54	71
Li <sub>4</sub> SiO <sub>4</sub> -based sorbents from fly ash-1 + 40 mol % K <sub>2</sub> CO <sub>3</sub>	600	600	10	2.27	2.27	71
Li <sub>4</sub> SiO <sub>4</sub> -based sorbents from fly ash-2 + 40 mol % K <sub>2</sub> CO <sub>3</sub>	600	600	5	1.36	1.36	71
Li <sub>4</sub> SiO <sub>4</sub> -based sorbents from fly ash-3 + 40 mol % K <sub>2</sub> CO <sub>3</sub>	600	600	5	1.31	0.88	71
Li <sub>4</sub> SiO <sub>4</sub> -qK (crystalline quartz + 10% mol K <sub>2</sub> CO <sub>3</sub> )	580	800	4	5	5.22	72
Li <sub>2</sub> ZrO <sub>3</sub>	650	650	8	1.5	1.82	19
Li <sub>2</sub> ZrO <sub>3</sub>	575	690	11	4.4	4.8	74
Li <sub>2</sub> ZrO <sub>3</sub>	500	650	3	1.63	1.63	66
Li <sub>2</sub> ZrO <sub>3</sub> (Li <sub>2</sub> CO <sub>3</sub> /K <sub>2</sub> CO <sub>3</sub> -doped)	550	800	6	1.3	1.3	65
Li <sub>2.2</sub> ZrO <sub>3.1</sub>	630	630	8	1.3	1.5	20
K <sub>0.2</sub> Li <sub>2</sub> ZrO <sub>3.1</sub>	630	630	8	1.17	1.27	20
K <sub>0.2</sub> Li <sub>1.6</sub> ZrO <sub>2.9</sub>	630	630	8	1.18	1.17	20
K <sub>0.6</sub> Li <sub>2.2</sub> ZrO <sub>3.4</sub>	630	630	8	1.17	0.65	20
K <sub>0.8</sub> Li <sub>2.2</sub> ZrO <sub>3.7</sub>	630	630	8	0.84	0.45	20
91.3% Li <sub>2</sub> ZrO <sub>3</sub> + 3.4% Y <sub>2</sub> O <sub>3</sub> + 0.2% Al <sub>2</sub> O <sub>3</sub> + 5.1% K <sub>2</sub> O	500	750	5	1.56	1.37	68
Li <sub>6</sub> Zr <sub>2</sub> O <sub>7</sub>	750	850	3	0.38	0.26	67
Li <sub>6</sub> Zr <sub>2</sub> O <sub>7</sub>	750	850	7	0.31	0.22	69
Li <sub>8</sub> ZrO <sub>6</sub>	750	850	4	3.6	2.41	67
Li <sub>8</sub> ZrO <sub>6</sub>	750	860	11	5.04	2.05	73
α-Li <sub>5</sub> AlO <sub>4</sub>	700	750	20	9.44	4.38	-
β-Li <sub>5</sub> AlO <sub>4</sub>	700	750	20	12.33	1.6	-

CO<sub>2</sub>. Therefore, after one cycle, Li<sub>2</sub>O is still found on the surface of the ceramic, and the ceramic is able to chemisorb CO<sub>2</sub> from the environment.

Table 2 summarizes the cyclability conditions for the different lithium ceramics reported in the literature, although there are other kinetic factors that must be taken into account to establish the best CO<sub>2</sub> absorption conditions for lithium ceramics. Figure 9 compares some of the cyclic stabilities reported for the following lithium ceramics: Li<sub>4</sub>SiO<sub>4</sub>, Li<sub>2</sub>ZrO<sub>3</sub>, Li<sub>6</sub>Zr<sub>2</sub>O<sub>7</sub>, Li<sub>8</sub>ZrO<sub>6</sub>, and Li<sub>5</sub>AlO<sub>4</sub> (results obtained in this work). As it can be seen from Table 2, most of these ceramics exhibit low CO<sub>2</sub> chemisorption capacities (between 0.4 and 4 mmol/g). However, both lithium aluminates polymorphs exhibit the highest CO<sub>2</sub> chemisorption capacities in a multicycle test. The α- and β-Li<sub>5</sub>AlO<sub>4</sub> phases seem to have some of the best cyclic CO<sub>2</sub> chemisorption/desorption behaviors, even compared to other lithium ceramics reported in the literature that were K-doped, which increases the CO<sub>2</sub> chemisorption properties. Therefore, if the lithium aluminates were K-doped, it would increase the CO<sub>2</sub> chemisorption rate because Li<sub>2</sub>CO<sub>3</sub> forms a eutectic phase with the K<sub>2</sub>CO<sub>3</sub> at high temperatures, resulting in a liquid shell that facilitates the diffusion of CO<sub>2</sub> throughout the product layer.<sup>71,72</sup>

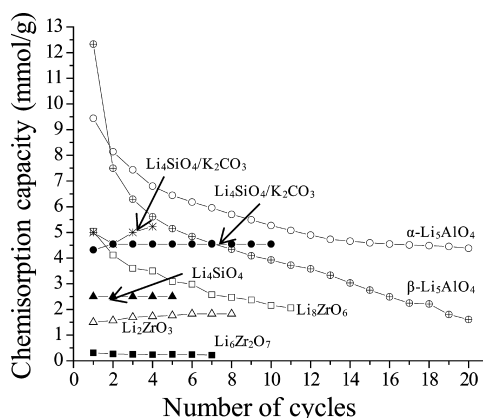


Figure 9. Cyclic stability of different lithium ceramics reported in the literature.<sup>19,69–71,73</sup>

#### 4. CONCLUSIONS

The α- and β-Li<sub>5</sub>AlO<sub>4</sub> polymorphs were synthesized using a solid-state reaction and then characterized by XRD and BET. The results indicate that the α-Li<sub>5</sub>AlO<sub>4</sub> phase is stable until 700 °C, and above this temperature, the polymorphic transformation into the β-Li<sub>5</sub>AlO<sub>4</sub> phase takes place. During the dynamic thermal analyses, both polymorphs showed similar trends and exhibited very high CO<sub>2</sub> chemisorptions. Both

lithium aluminate polymorphs are able to chemisorb CO<sub>2</sub> in a wide temperature range, from 210 to 690 °C, but the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase only chemisorbed 53.14 wt %, whereas the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase chemisorbed 67.21 wt %. As it has been mentioned in previous papers, powder lithium ceramics tend to sinter, which produces an important decrease in the surface area, reducing the CO<sub>2</sub> chemisorption. To avoid the sintering effect and to perform a correct kinetic analysis, samples were homogeneously sintered prior to performing the isothermal experiments. All isotherms were fit to a double exponential model because it can describe two different processes: (1) the CO<sub>2</sub> chemisorption over the surface of the Li<sub>5</sub>AlO<sub>4</sub> particles and (2) the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes. The kinetic constant values indicated that the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes is the rate-limiting step for the whole process. Additionally, by fitting these data to Eyring's model, the  $\Delta H^\ddagger$  values were obtained that indicate that the CO<sub>2</sub> direct chemisorption process is more dependent on temperature than the CO<sub>2</sub> chemisorption kinetically controlled by diffusion processes, at least between 600 and 675 °C. The cyclic performance tests indicate that both lithium aluminates polymorphs exhibit a gradually reduced chemisorption capacity during the multicycle processes, perhaps due to the sublimation of the Li<sub>2</sub>O during the desorption process, resulting in a reduction in the CO<sub>2</sub> chemisorption capacity. The CO<sub>2</sub> chemisorption capacity in the  $\alpha$ -Li<sub>5</sub>AlO<sub>4</sub> phase is higher than that of the  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phase after 20 cycles. Finally, the  $\alpha$ - and  $\beta$ -Li<sub>5</sub>AlO<sub>4</sub> phases appear to have some of the best cyclic CO<sub>2</sub> chemisorption/desorption behaviors, even compared to other lithium ceramics that have been K-doped, increasing their CO<sub>2</sub> chemisorption efficiencies.

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### Notes

The authors declare no competing financial interest.

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