

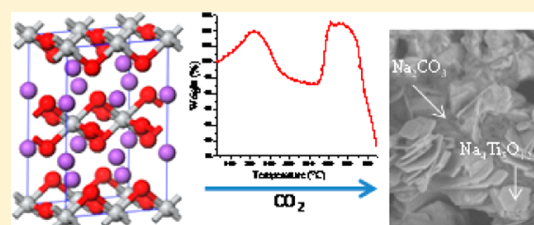
# Thermodynamic and Kinetic Analyses of the CO<sub>2</sub> Chemisorption Mechanism on Na<sub>2</sub>TiO<sub>3</sub>: Experimental and Theoretical Evidences

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**ABSTRACT:** Sodium metatitanate (Na<sub>2</sub>TiO<sub>3</sub>) was successfully synthesized via a solid-state reaction. The Na<sub>2</sub>TiO<sub>3</sub> structure and microstructure were characterized using X-ray diffraction, scanning and transmission electron microscopy, and N<sub>2</sub> adsorption. Then, the CO<sub>2</sub> chemisorption mechanism on Na<sub>2</sub>TiO<sub>3</sub> was systematically analyzed to determine the influence of temperature. The CO<sub>2</sub> chemisorption capacity of Na<sub>2</sub>TiO<sub>3</sub> was evaluated both dynamically and isothermally, and the products were reanalyzed to elucidate the Na<sub>2</sub>TiO<sub>3</sub>-CO<sub>2</sub> reaction mechanism. Different chemical species (Na<sub>2</sub>CO<sub>3</sub>, Na<sub>2</sub>O, and Na<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> or Na<sub>16</sub>Ti<sub>10</sub>O<sub>28</sub>) were identified during the CO<sub>2</sub> capture process in Na<sub>2</sub>TiO<sub>3</sub>. In addition, some CO<sub>2</sub> chemisorption kinetic parameters were determined. The ΔH<sup>‡</sup> was found to be 140.9 kJ/mol, to the Na<sub>2</sub>TiO<sub>3</sub>-CO<sub>2</sub> system, between 600 and 780 °C. Results evidenced that CO<sub>2</sub> chemisorption on Na<sub>2</sub>TiO<sub>3</sub> highly depends on the reaction temperature. Furthermore, the experiments were theoretically supported by different thermodynamic calculations. The calculated thermodynamic properties of CO<sub>2</sub> capture reactions by (Na<sub>2</sub>TiO<sub>3</sub>, Na<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>, and Na<sub>16</sub>Ti<sub>10</sub>O<sub>28</sub>) sodium titanates were fully investigated.



## I. INTRODUCTION

Carbon dioxide (CO<sub>2</sub>) emissions are one of the most threatening pollution problems in the world. One approach to solve such an environmental problem is CO<sub>2</sub> capture and storage.<sup>1–3</sup> The capture of CO<sub>2</sub> emissions, at stationary point sources (e.g., power stations, smelters, and refineries), is considered a key technology for achieving greenhouse gas reductions. Nevertheless, the selection of the best CO<sub>2</sub> sorbent is not a simple task, as the typical operating temperatures involved are considerably high (500–900 °C), which would rule out the majority of traditional carbon dioxide sorbents, for example, polymer-based membrane materials and amine solution.<sup>4</sup> Therefore, CO<sub>2</sub> capture and storage in solid materials have been considered to be the most practical option as an efficient and cheap alternative to reduce greenhouse gases. In this way, different materials have been proposed as CO<sub>2</sub> captors such as zeolites, porous (active) carbons, metal–organic frameworks (MOFs), alkali metal-promoted alumina and carbonates, alkaline and alkaline-earth ceramics, and layered double hydroxides.<sup>5</sup> These materials are reported to be capable of CO<sub>2</sub> capture at moderate and/or high temperatures.

Among these materials, different alkaline ceramics have been reported as good solid candidates for CO<sub>2</sub> sorbents in terms of large CO<sub>2</sub> sorption capacity and high operating temperatures.<sup>5–79</sup> Some of the alkaline ceramics most studied are lithium silicates (Li<sub>8</sub>SiO<sub>6</sub>, Li<sub>4</sub>SiO<sub>4</sub>, and Li<sub>2</sub>SiO<sub>3</sub>),<sup>6–34</sup> lithium zirconates (Li<sub>8</sub>ZrO<sub>6</sub>, Li<sub>6</sub>ZrO<sub>7</sub>, and Li<sub>2</sub>ZrO<sub>3</sub>),<sup>32,35–59</sup> lithium aluminate (Li<sub>3</sub>AlO<sub>4</sub>),<sup>60–63</sup> sodium silicate (Na<sub>2</sub>SiO<sub>3</sub>),<sup>64</sup> lithium cuprate (Li<sub>2</sub>CuO<sub>2</sub>),<sup>65–68</sup> and sodium zirconate

(Na<sub>2</sub>ZrO<sub>3</sub>),<sup>69–79</sup> among other ceramics. All these ceramics are able to trap CO<sub>2</sub> chemically, through a similar reaction mechanism: Initially, CO<sub>2</sub> is chemisorbed over the ceramic surface, which implies the formation of an external shell. The external shell is composed of the corresponding alkaline carbonate (Li<sub>2</sub>CO<sub>3</sub> or Na<sub>2</sub>CO<sub>3</sub>) as well as secondary phases and/or metal oxides. Once the superficial external shell is complete, the CO<sub>2</sub> chemisorption can be reactivated if the temperature is increased sufficiently to allow different diffusion processes. Therefore, CO<sub>2</sub> chemisorption is reactivated throughout CO<sub>2</sub> diffusion on mesopore structures (if the external shell contains mesopores)<sup>72</sup> or throughout bulk intercrystalline atomic diffusion processes on these materials.<sup>80</sup>

Alternately, there are several sodium titanates reported in the literature that have been synthesized by different methods<sup>81–83</sup> and used in different applications such as a basic catalyst in transesterification reactions, water splitting reactions, and on different ferroelectric properties.<sup>84–86</sup> However, there is only one report about the use of sodium metatitanate (Na<sub>2</sub>TiO<sub>3</sub>) as a possible CO<sub>2</sub> captor. López-Ortiz et al.,<sup>79</sup> synthesized and tested different sodium ceramics as CO<sub>2</sub> captors. Sodium metatitanate (Na<sub>2</sub>TiO<sub>3</sub>) was one of these sodium ceramics, but unfortunately only one CO<sub>2</sub> isothermal experiment was performed at 600 °C. There is not enough information about the CO<sub>2</sub> chemisorption mechanism on sodium titanate,

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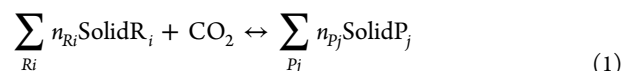
$\text{Na}_2\text{TiO}_3$ . The aim of the present work is to systematically analyze the  $\text{CO}_2$  chemisorption mechanism on  $\text{Na}_2\text{TiO}_3$  as a function of temperature. The  $\text{CO}_2$  chemisorption capacity of  $\text{Na}_2\text{TiO}_3$  was evaluated dynamically and isothermally to determine the influence of temperature on the  $\text{Na}_2\text{TiO}_3$ – $\text{CO}_2$  reaction mechanism and kinetic behavior. Additionally, the experiments were theoretically supported by different thermodynamic calculations.

## II. EXPERIMENTAL SECTION

$\text{Na}_2\text{TiO}_3$  was synthesized via a solid-state reaction. It was obtained by mixing mechanically the corresponding amounts of titanium oxide ( $\text{TiO}_2$ , Aldrich) and sodium carbonate ( $\text{Na}_2\text{CO}_3$ , Aldrich), with a  $\text{Na}_2\text{CO}_3/\text{TiO}_2$  molar ratio of 1.1:1. Powders were mixed and subsequently calcined at  $850\text{ }^\circ\text{C}$  for 12 h. After the solid-state synthesis,  $\text{Na}_2\text{TiO}_3$  was structural and microstructurally characterized, before and after the  $\text{CO}_2$  capture process, using powder X-ray diffraction (XRD), scanning (SEM), and transmission (TEM) electron microscopies, and  $\text{N}_2$  adsorption–desorption. XRD patterns were obtained with a D8 Bruker diffractometer coupled to a Cu anode X-ray tube in Bragg–Brentano configuration. The  $K\alpha_1$  wavelength was selected with a diffracted beam Ge monochromator, and the compounds were identified conventionally using the Joint Committee Powder Diffraction Standards (JCPDS) database. The experimental error was  $\pm 3\%$ . Then,  $\text{Na}_2\text{TiO}_3$  textural characteristics (surface area and porosity) were determined using  $\text{N}_2$  adsorption/desorption. For the  $\text{N}_2$  adsorption/desorption experiments, the isotherms were acquired on a Bel-Japan Minisorp II at 77 K using a multipoint technique. Previously, the samples were degassed at room temperature for 24 h under vacuum prior to analysis. Scanning and transmission electron microscope images were obtained from JMS-7600F and JEM-1200EX JEOL equipment, respectively. In both cases, the sample preparation was performed by standard procedures.

Different  $\text{CO}_2$  chemisorption experiments were performed using Q500HR equipment, from TA Instruments. Initially,  $\text{Na}_2\text{TiO}_3$  was dynamically heated from room temperature to  $850\text{ }^\circ\text{C}$  at  $5\text{ }^\circ\text{C}/\text{min}$ . These analyses were carried out under an excess  $\text{CO}_2$  atmosphere (Praxair, grade 3.0), using a 60 mL/min of gas flow. A saturated  $\text{CO}_2$  atmosphere (100 wt %) was used in order to determine the viability of  $\text{Na}_2\text{TiO}_3$  as  $\text{CO}_2$  captor. For the isothermal analyses, fresh sample was heated at its respective isothermal temperature (between 300 and  $700\text{ }^\circ\text{C}$ ) under a  $\text{N}_2$  flow (Praxair, grade 4.8). When the sample reached the corresponding temperature, the gas flow was switched from  $\text{N}_2$  to  $\text{CO}_2$  (60 mL/min) throughout the duration of the experiment. To elucidate the  $\text{Na}_2\text{TiO}_3$ – $\text{CO}_2$  capture mechanism, products obtained from the isothermal analyses were recharacterized using XRD, SEM, and TEM.

Since the thermodynamic properties of the sodium titanates ( $\text{Na}_4\text{Ti}_5\text{O}_{12}$ ,  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$ ) are not available in the literature, we performed the *ab initio* thermodynamics calculations on these sodium titanates by combining density functional theory (DFT) with lattice phonon dynamics. For comparison reasons, the thermodynamic properties of  $\text{Na}_2\text{TiO}_3$  were also calculated and compared with the known experimental data. The detailed descriptions of the calculation method can be found in previous studies.<sup>29,87,88</sup> The  $\text{CO}_2$  capture reactions of sodium titanate solids can be expressed generically in the form (for convenient description, we normalized the reaction to 1 mol of  $\text{CO}_2$ )



where  $n_{R_i}$ ,  $n_{P_j}$  are the reactants ( $R_i$ ) and products ( $P_j$ ) moles involved in the capture reactions. We treat the gas phase  $\text{CO}_2$  as an ideal gas. By assuming that the difference between the Gibbs free energy ( $\Delta G^\circ$ ) of the solid phases of reactants ( $R_i$ ) and products ( $P_j$ ) can be approximated by the difference in their total energies ( $\Delta E_{\text{DFT}}$ ), obtained directly from DFT calculations, and the vibrational free energy of the phonons and by ignoring the PV contribution terms for solids, the variation of the chemical potential ( $\Delta\mu$ ) for reaction 1 with temperature and pressure can be written as

$$\Delta G(T, P) = \Delta G^\circ(T) - RT \ln \frac{P_{\text{CO}_2}}{P_0} \quad (2)$$

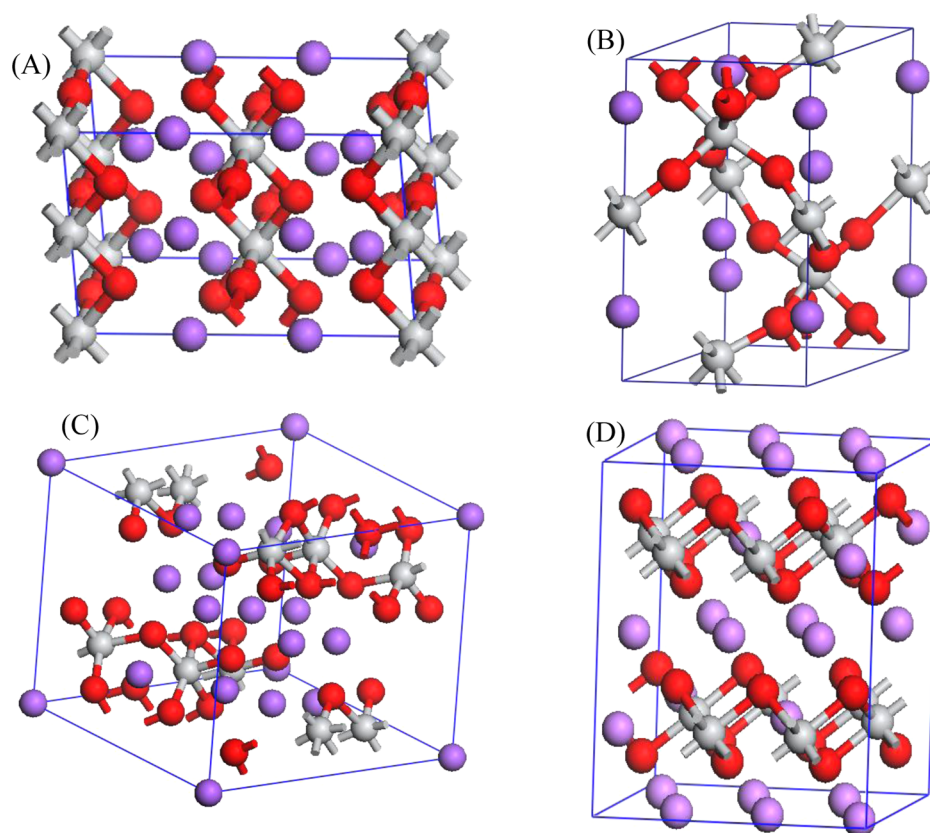
where,

$$\Delta G^\circ(T) \approx \Delta E_{\text{DFT}} + \Delta E_{\text{ZP}} + \Delta F_{\text{PH}}(T) - G_{\text{CO}_2}^0(T) \quad (3)$$

Here,  $\Delta E_{\text{DFT}}$  is the DFT energy difference between the reactants and products of the reaction 1,  $\Delta E_{\text{ZP}}$  is the zero-point energy difference between the reactants and products and can be obtained directly from phonon calculations.  $\Delta F_{\text{PH}}$  is the phonon free energy change excluding zero-point energy (which is already counted into the  $\Delta E_{\text{ZP}}$  term) between the solids of products and reactants.  $P_{\text{CO}_2}$  is the partial pressure of  $\text{CO}_2$  in the gas phase, and  $P_0$  is the standard state reference pressure taken to be 1 bar. The heat of reaction ( $\Delta H^{\text{cal}}(T)$ ) can be evaluated through the following equation:

$$\Delta H^{\text{cal}}(T) = \Delta G^\circ(T) + T[\Delta S_{\text{PH}}(T) - S_{\text{CO}_2}(T)] \quad (4)$$

where,  $\Delta S_{\text{PH}}(T)$  is the difference of entropies between product solids and reactant solids. The free energy of  $\text{CO}_2$  ( $G_{\text{CO}_2}^0$ ) can be obtained from standard statistical mechanics,<sup>87–89</sup> and its entropy ( $S_{\text{CO}_2}$ ) can be found in the empirical thermodynamic databases.<sup>90</sup> First-principles density-functional theory calculations with plane-wave basis sets and pseudopotential approximation were done to describe the structural, energetic, and electronic properties of sodium titanates considered in this study. All calculations were performed using the Vienna *ab initio* simulation package (VASP).<sup>91,92</sup> In this study, the PAW pseudopotentials and PW91 exchange-correlation functional were used in all of the calculations. Plane wave basis sets were used with a kinetic energy cutoff of 520 eV and an augmentation charge cutoff of 605.4 eV. The k-point sampling grids of  $m \times n \times l$ , obtained using the Monkhorst–Pack method,<sup>93</sup> are used for these bulk calculations, where  $m$ ,  $n$ , and  $l$  are determined with a spacing of about  $0.028\text{ \AA}^{-1}$  along the reciprocal axes of their unit cells. In the phonon calculations, a  $4 \times 3 \times 2$  supercell of  $\text{Na}_2\text{TiO}_3$ , a  $2 \times 2 \times 1$  supercell of  $\text{Na}_4\text{Ti}_5\text{O}_{12}$ , and a  $2 \times 2 \times 2$  supercell of  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$  were created from their optimized unit cells which were calculated through DFT. The displacement of  $0.03\text{ \AA}$  of nonequivalent atoms is generated. Then, for each supercell, the DFT calculations were performed again to obtain the force on each atom due to the displacements. These forces are carried back to PHONON package<sup>94</sup> to calculate the phonon dispersions and densities from which the partition function can be carried out.



**Figure 1.** Crystal structures of different sodium titanates and sodium zirconate: (A)  $\text{Na}_2\text{TiO}_3$  in space group  $Immm$  (No. 71), (B)  $\text{Na}_4\text{Ti}_5\text{O}_{12}$  in space group  $P3$  (No. 143), (C)  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$  in space group  $P\bar{1}$  (No. 2), and (D)  $\text{Na}_2\text{ZrO}_3$  in space group  $C2/c1$  (No. 15). Red stands for oxygen, purple stands for sodium, and gray stands for titanium or zirconium.

**Table 1.** Experimental and Optimized Crystal Structural Constants of Different Sodium Titanates and Sodium Zirconate. The Calculated Energy ( $E_{\text{DFT}}$ ), the Zero-Point Energy ( $E_{\text{zp}}$ ), and Entropy at  $T = 300$  K Are Also Listed

crystal and space group	experiment	optimized and deviation (%)	$E_{\text{DFT}}$ (eV/f.u.)	$E_{\text{zp}}$ (kJ/mol)	Entropy (J/mol·K)
$\text{Na}_2\text{TiO}_3$ $Immm$ (No. 71) <sup>a</sup> $Z = 2$	$a = 9.535 \text{ \AA}$ $b = 4.495 \text{ \AA}$ $c = 3.178 \text{ \AA}$	10.07599 (5.67%) 4.22818 (−5.94%) 3.01881 (−5.01%)	−39.01091	35.493	115.979
$\text{Na}_4\text{Ti}_5\text{O}_{12}$ $P3$ (No. 143) <sup>b</sup> $Z = 1$	$a = 5.31997 \text{ \AA}$ $c = 9.5567 \text{ \AA}$ $\gamma = 120^\circ$	5.35915 (0.74%) 9.63762 (0.85%) 120 (0%)	−159.60844	129.348	409.775
$\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$ $P\bar{1}$ (No. 2) <sup>c</sup> $Z = 1$	$a = 10.51 \text{ \AA}$ $b = 8.34 \text{ \AA}$ $c = 8.53 \text{ \AA}$ $\alpha = 112.63^\circ$ $\beta = 104.1^\circ$ $\gamma = 102.19^\circ$	10.57946 (0.66%) 8.39552 (0.67%) 8.57695 (0.55%) 112.485 (−0.12%) 104.210 (0.11%) 102.092 (−0.01%)	−371.65981	324.737	1072.428
$\text{Na}_2\text{ZrO}_3$ $C12/c1$ (No. 15) <sup>d</sup> $Z = 8$	$a = 5.63 \text{ \AA}$ $b = 9.749 \text{ \AA}$ $c = 11.127 \text{ \AA}$ $\beta = 99.98^\circ$	5.61281 (−0.18%) 9.73575 (−0.14%) 10.95675 (−1.53%) 100.043 (0.01%)	−41.56924	34.497	119.319

<sup>a</sup>From ref 95. <sup>b</sup>From ref 96. <sup>c</sup>From ref 97. <sup>d</sup>From ref 98.

### III. RESULTS AND DISCUSSION

The crystal structures of Na-rich sodium titanates studied here are shown in Figure 1 and their experimental and optimized crystal parameters are listed in Table 1. As Liu et al.<sup>86</sup> reported, the  $\text{Na}_2\text{TiO}_3$  has a NaCl-type structure with space group  $Immm$  (No. 71) as shown in Figure 1A. The other two Na-rich sodium titanates ( $\text{Na}_4\text{Ti}_5\text{O}_{12}$  and  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$ ) possess the following

space groups  $P3$  (No. 143) and  $P\bar{1}$  (No. 2), and they are shown in Figure 1 panels B and C. For comparison reasons, the structure of  $\text{Na}_2\text{ZrO}_3$  ( $C12/c1$  (No. 15)) is also shown in Figure 1D and described in Table 1.

$\text{Na}_2\text{TiO}_3$  was synthesized via a solid state reaction, and the corresponding XRD pattern is shown in Figure 2. The XRD pattern fits very well with the 00-050-0110 PDF file, which

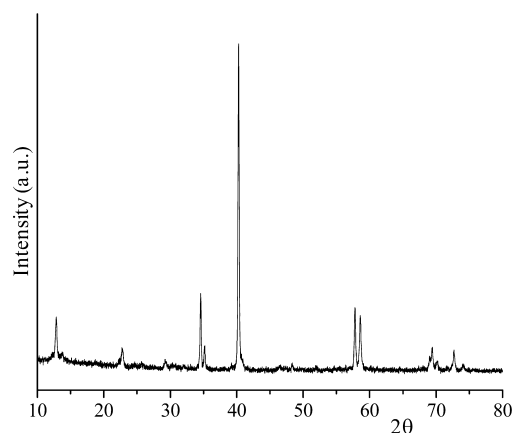


Figure 2. XRD pattern of the  $\text{Na}_2\text{TiO}_3$  sample.

corresponds to the  $\text{Na}_2\text{TiO}_3$  phase. After the structural identification, the  $\text{N}_2$  adsorption–desorption isotherm and SEM analysis for the  $\text{Na}_2\text{TiO}_3$  sample were acquired to determine some microstructural characteristics. Figure 3 shows

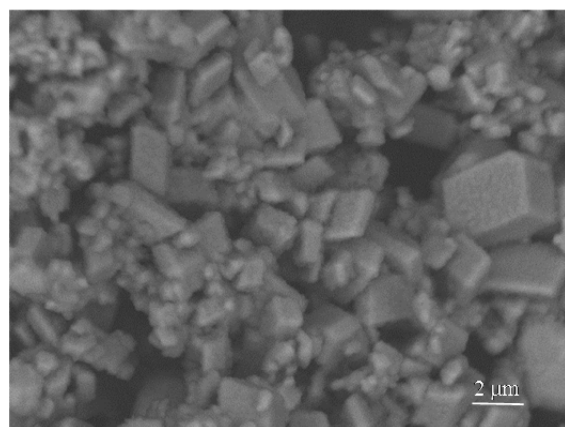
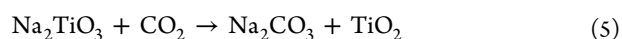


Figure 3. Backscattered electron image of the  $\text{Na}_2\text{TiO}_3$  sample.

some of the morphological characteristics of the  $\text{Na}_2\text{TiO}_3$  sample.  $\text{Na}_2\text{TiO}_3$  sample formed well-defined polyhedral particles which varied their size from 200 to 300 nm up to 3–4  $\mu\text{m}$ . These particles structured nondense agglomerates of 30–50  $\mu\text{m}$  in size. To complement the  $\text{Na}_2\text{TiO}_3$  microstructural characterization, it was analyzed by  $\text{N}_2$  adsorption. The  $\text{N}_2$  adsorption–desorption curve corresponds to a type II isotherm according to the IUPAC classification (data not shown). The isotherm did not present hysteresis. This behavior corresponds to a nonporous, dense aggregate of particles. Additionally, the surface area of the sample was estimated to be 0.8  $\text{m}^2/\text{g}$ , using the BET model.

To further analyze and test this material,  $\text{CO}_2$  chemisorption was studied. According to previous works based on sodium and lithium ceramics, a complete reaction between  $\text{Na}_2\text{TiO}_3$  and  $\text{CO}_2$  would be expected to follow the reaction 5:



In fact, as it was described at the Introduction section, there is only one previous paper in which the  $\text{CO}_2$  capture in  $\text{Na}_2\text{TiO}_3$  was tested.<sup>79</sup> Unfortunately, in that paper the  $\text{CO}_2$  capture process was only isothermally evaluated at 600 °C. Thus, the

$\text{CO}_2$ – $\text{Na}_2\text{TiO}_3$  system has not been totally analyzed as a function of temperature.

Figure 4 shows the dynamic thermogram of  $\text{Na}_2\text{TiO}_3$  into a  $\text{CO}_2$  flow. In this case, the thermogram did not present the

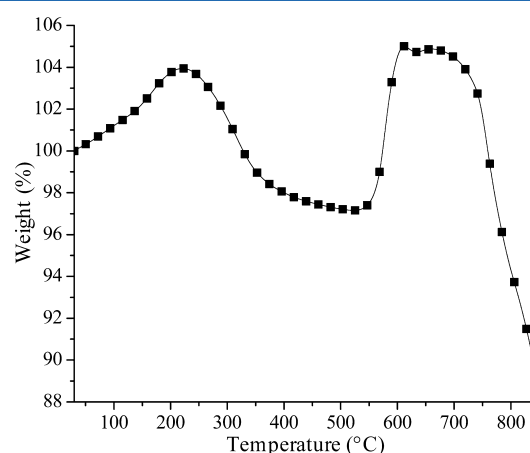
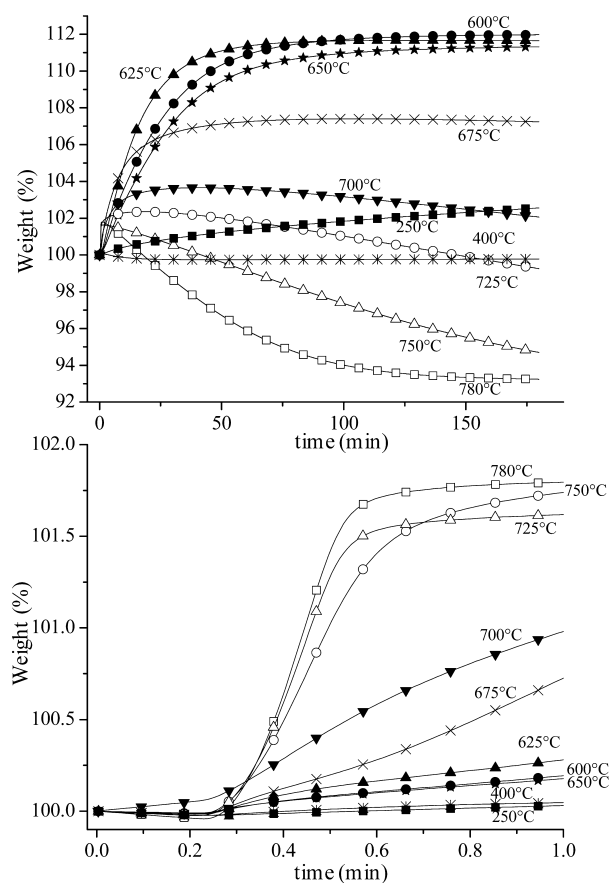


Figure 4. Dynamic thermogravimetric analysis of the  $\text{Na}_2\text{TiO}_3$  sample into a  $\text{CO}_2$  flux.

typical behavior observed for other lithium and sodium ceramics.<sup>72,80</sup> In this case, there is a continuous weight gain between 30 and 225 °C. The maximum weight increment observed at 225 °C was equal to 3.9 wt %. After that, between 230 and 524 °C the thermogram showed a weight decrement of 6.7 wt %. This means that the  $\text{Na}_2\text{TiO}_3$  sample lost even more weight than that gained previously. Then, a sudden second weight increment was produced between 530 and 610 °C. Here, the total weight increment was equal to 8 wt %. After this weight increment, the weight did not vary until 700 °C, a temperature at which the weight began to decrease. In fact, the last weight decrement went up to only 88 wt % of the initial weight. In other words, the  $\text{Na}_2\text{TiO}_3$  sample lost 12 wt %.

In general, lithium and sodium ceramics present one or two consecutive weight increments associated with the superficial and bulk  $\text{CO}_2$  chemisorption process followed from a final weight increment, which is similar to the previously weight gained.<sup>72,80</sup> Only in some cases, a weight decrement between the two weight increments has been reported, and it has been associated with a superficial  $\text{CO}_2$  chemisorption–desorption equilibrium.<sup>75</sup> In those cases, the weight decrement never was equal or higher than the initial weight increment. Nevertheless, in the  $\text{Na}_2\text{TiO}_3$  case, both weight increments are associated with sequential weight decrements, which are higher than the previous increments. Hence, it seems that  $\text{Na}_2\text{TiO}_3$  possesses a different  $\text{CO}_2$  capture reaction mechanism, depending on temperature, and its thermal stability is not as high as in the ceramics previously reported. Therefore, different isothermal experiments were performed, and the products obtained from those isotherms were recharacterized by XRD, SEM, and TEM.

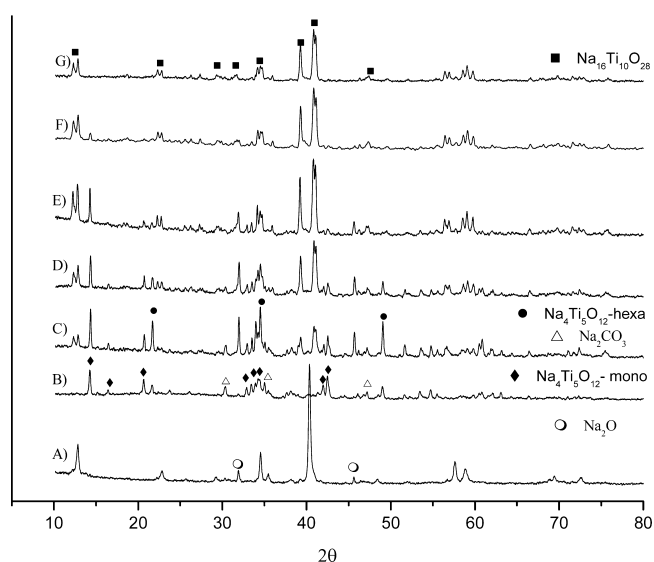
Figure 5 shows the  $\text{Na}_2\text{TiO}_3$  isotherms obtained at different temperatures into a  $\text{CO}_2$  flow. The initial isothermal experiment was performed at 250 °C, as the first maximum weight increment was at a similar temperature. This isotherm did not reach the equilibrium after 3 h and the weight increase was only 2.6 wt %. The second isotherm was performed at 400 °C, where the first weight decrement is significantly evidenced. This isotherm did not seem to present any important weight increment, as only less than 0.1 wt % of  $\text{CO}_2$  was captured in



**Figure 5.**  $\text{Na}_2\text{TiO}_3$ - $\text{CO}_2$  chemisorption isotherms at different temperatures: complete isotherms (A) and first minute of the same isotherms (B).

the first seconds, but this  $\text{CO}_2$  was immediately desorbed. Kinetically, the insipient  $\text{CO}_2$  capture was faster at 400 °C than at 250 °C only during the first minute (Figure 5B). This behavior would be expected from the previous dynamic TG experiment. Between 600 and 650 °C isotherms presented the typical exponential behavior, gaining ~11.5 wt % (efficiency of 40%). In fact the maximum weight increment (11.9 wt %) was observed at 600 °C, although the  $\text{CO}_2$  chemisorption was faster at higher temperatures, up to 780 °C (Figure 5B). However, the isotherms performed between 675 and 780 °C decreased their final weights. At 675 and 700 °C the final weight increments were 7.2 and 2.0 wt % respectively, evidencing that a  $\text{CO}_2$  chemisorption-desorption equilibrium was activated and favored as a function of temperature. Additionally, isotherms performed at  $T > 700$  °C presented final weight decrements (wt % < 100%), although these isotherms presented weight increment during the first minutes. For example, the isotherm performed at 750 °C gained 1.6 wt % in the first 3 min, but after 3 h the isotherm final weight was equal to -5.3 wt %. Of course, these results clearly showed that not only  $\text{CO}_2$  has been desorbed at high temperatures, but also part of the  $\text{Na}_2\text{TiO}_3$  is being decomposed.

To elucidate the  $\text{CO}_2$ - $\text{Na}_2\text{TiO}_3$  chemisorption mechanism, as a function of temperature, the isothermal products were analyzed by XRD, SEM, and TEM. Figure 6 shows the XRD patterns of all  $\text{CO}_2$ - $\text{Na}_2\text{TiO}_3$  isothermal products, and a pristine  $\text{Na}_2\text{TiO}_3$  pattern was included for comparison purposes. The 250 and 400 °C sample products evidenced the prevalence of the  $\text{Na}_2\text{TiO}_3$  phase (00-050-0110 PDF file),

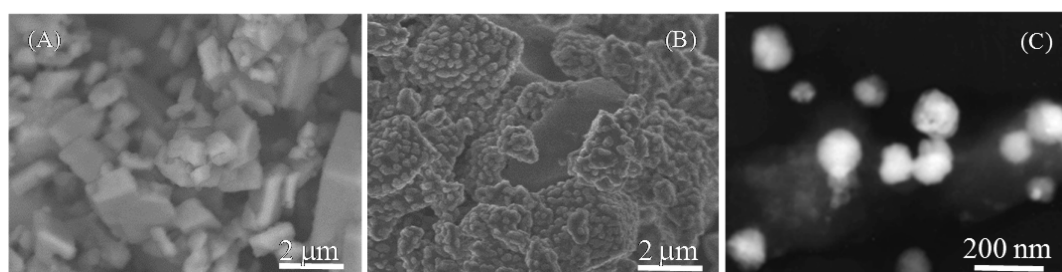


**Figure 6.** XRD patterns of the  $\text{Na}_2\text{TiO}_3$ - $\text{CO}_2$  products treated isothermally at different temperatures. (A) 250, (B) 650, (C) 675, (D) 700, (E) 725, (F) 750, (G) 780 °C.

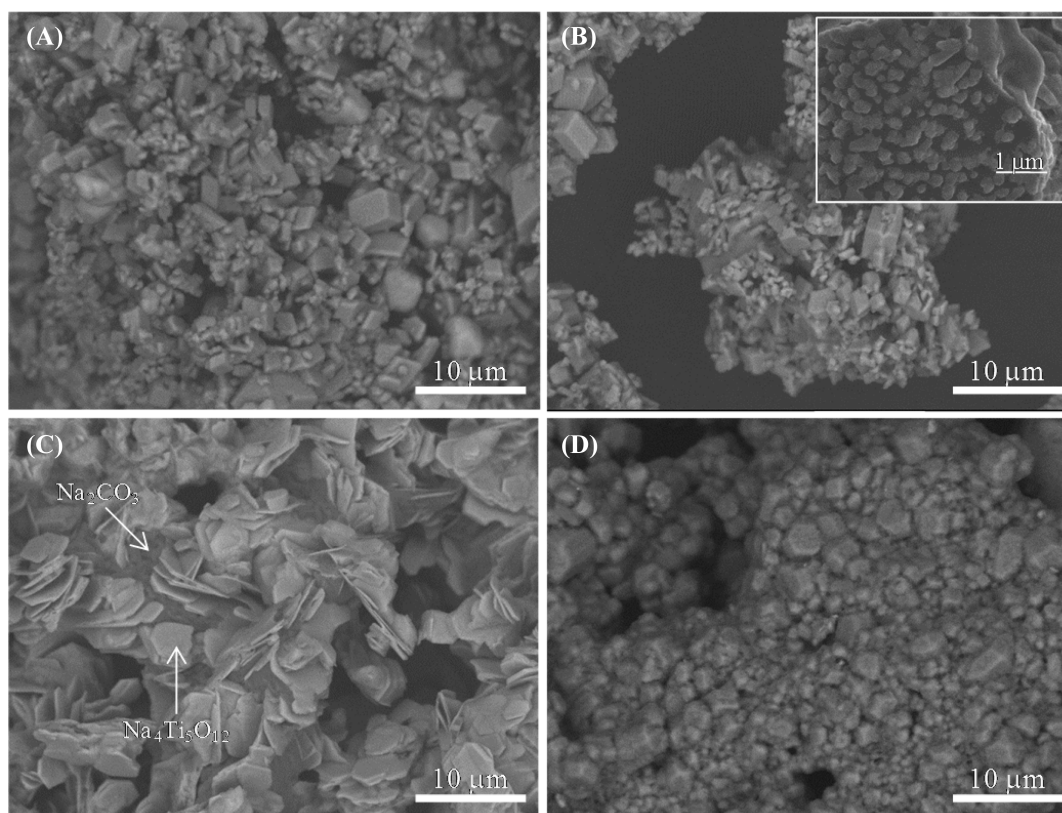
as it could be expected. Nevertheless, new and well-defined peaks appeared at 27.5°, 31.8°, 45.6°, 56.5°, and 75.3° in  $2\theta$ . In fact, the intensity of these new peaks increased as a function of temperature. Sodium carbonate ( $\text{Na}_2\text{CO}_3$ ) was not detected as the  $\text{CO}_2$  chemisorption was almost negligible at these temperatures, but the new diffraction peaks fit to cubic sodium oxide phase ( $\text{Na}_2\text{O}$ , 96-900-9064 PDF file). Thus, in this temperature range 250–400 °C,  $\text{CO}_2$  is initially chemisorbed on  $\text{Na}_2\text{TiO}_3$ , which must produce  $\text{Na}_2\text{CO}_3$ . However,  $\text{CO}_2$  is desorbed after some minutes, leaving the sodium atoms as  $\text{Na}_2\text{O}$  over the  $\text{Na}_2\text{TiO}_3$  particle surfaces. This relatively low temperature range (250–400 °C) must not allow the sodium diffusion, and its reincorporation into the  $\text{Na}_2\text{TiO}_3$  phase. Moreover, the  $\text{Na}_2\text{TiO}_3$  must tolerate a partial sodium extraction without being destabilized because of its layered crystalline structure.<sup>83</sup>

To complement the XRD results related to the  $\text{Na}_2\text{O}$  formation, SEM and TEM characterizations were performed. Figure 7 shows different morphological aspects of the  $\text{Na}_2\text{TiO}_3$ - $\text{CO}_2$  product obtained at 400 °C. In general, the morphology of this sample did not seem to present important variations in comparison to the original  $\text{Na}_2\text{TiO}_3$  sample (see Figure 3), as it can be seen in the backscattered image (Figure 7A). The sample presented well-defined polyhedral particles of around 2–3  $\mu\text{m}$ . However, the secondary electron image evidenced important changes in the  $\text{Na}_2\text{TiO}_3$  particle surfaces (Figure 7B). It is clear that the  $\text{Na}_2\text{TiO}_3$  sample formed a corrugated surface produced by the formation of tiny spherical-like structures. In fact, these spherical-like structures were confirmed through a TEM analysis (Figure 7C), where a particle size of ~100 nm was determined. Of course, the formation of these nanoparticles should be related to the  $\text{Na}_2\text{O}$  formation, which was previously evidenced by XRD.

Coming back to the XRD results presented (Figure 6), the patterns corresponding to the isothermal products obtained between 600 and 780 °C showed the formation of different phases. As it could be expected,  $\text{Na}_2\text{CO}_3$  was produced due to the  $\text{CO}_2$  chemisorption. However,  $\text{Na}_2\text{TiO}_3$  did not totally react according to eq 1, in which  $\text{Na}_2\text{CO}_3$  and  $\text{TiO}_2$  would be produced. Here, a different sodium titanate was produced,

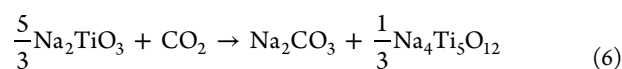


**Figure 7.** Electron microscope analysis of the  $\text{Na}_2\text{TiO}_3$  sample treated at  $400\text{ }^\circ\text{C}$  into a  $\text{CO}_2$  flux. Backscattered scanning electron (A), secondary scanning electron (B), and bright field transmission electron images (C).



**Figure 8.** Scanning electron images of pristine  $\text{Na}_2\text{TiO}_3$  (A) and  $\text{Na}_2\text{TiO}_3\text{-CO}_2$  isothermal products obtained at  $400$  (B),  $600$  (C), and  $750\text{ }^\circ\text{C}$  (D).

$\text{Na}_4\text{Ti}_5\text{O}_{12}$ . It means that  $\text{Na}_2\text{TiO}_3$  only reacts partially with  $\text{CO}_2$ , in this temperature range ( $600\text{--}650\text{ }^\circ\text{C}$ ), according to the following reaction:

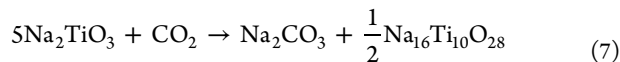


Moreover, two other issues must be pointed out from these XRD patterns. The  $\text{Na}_4\text{Ti}_5\text{O}_{12}$  crystalline phase changes from monoclinic to hexagonal, when temperature is increased from  $650$  to  $675\text{ }^\circ\text{C}$  and  $\text{Na}_2\text{O}$  appears at  $675\text{ }^\circ\text{C}$ . The  $\text{Na}_4\text{Ti}_5\text{O}_{12}$  phase change can be related to different thermal stabilities. On the contrary, the  $\text{Na}_2\text{O}$  formation may be related to the  $\text{CO}_2$  desorption process. However, at these temperatures sodium should not have diffusion problems to regenerate the  $\text{Na}_2\text{TiO}_3$  phase, as it has been probed for other sodium ceramics, such as  $\text{Na}_2\text{ZrO}_3$ .<sup>72</sup> However, the secondary sodium titanate phase ( $\text{Na}_4\text{Ti}_5\text{O}_{12}$ ) possesses a denser crystalline structure ( $2.2\text{ g/cm}^3$ ) than  $\text{Na}_2\text{TiO}_3$  ( $1.8\text{ g/cm}^3$ ), which may inhibit the sodium diffusion and consequently the  $\text{Na}_2\text{TiO}_3$  regeneration.

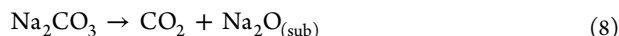
The crystal structures of these sodium titanates are quite different. In  $\text{Na}_2\text{TiO}_3$ , each Ti is coordinated with six oxygen atoms and each oxygen binds with two Ti atoms to form a  $\text{TiO}_3$  plane (Figure 1A). Along the  $\langle 100 \rangle$  direction, between  $[\text{TiO}_3]$  planes, there are two Na layers interacting with the oxygen atoms of the  $[\text{TiO}_3]$  planes. Interestingly, the crystal structure of  $\text{Na}_2\text{TiO}_3$  is different with  $\text{Na}_2\text{ZrO}_3$  as shown in Figure 1D. However, in the  $\text{Na}_4\text{Ti}_5\text{O}_{12}$  structure (Figure 1B), each  $[\text{TiO}_4]$  tetrahedral chain is surrounded by Na atoms, and in  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$  (Figure 1C), each Ti coordinates with five oxygen atoms in which only one binds perpendicular with Ti of  $[\text{TiO}_5]$ , another two pair of oxygen atoms bind with two Ti of neighboring  $[\text{TiO}_5]$  clusters. Obviously, different structures result in different electronic and thermodynamic properties.

At temperatures higher than  $650\text{ }^\circ\text{C}$   $\text{Na}_2\text{CO}_3$ ,  $\text{Na}_4\text{Ti}_5\text{O}_{12}$ , and  $\text{Na}_2\text{O}$  tended to disappear, while  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$  appears as a function of temperature. Therefore, XRD patterns and isothermal results show that the  $\text{CO}_2\text{-Na}_2\text{TiO}_3$  interaction is weakened if the temperature is increased. In fact,  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$  was the only phase detected at  $780\text{ }^\circ\text{C}$ . The  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$

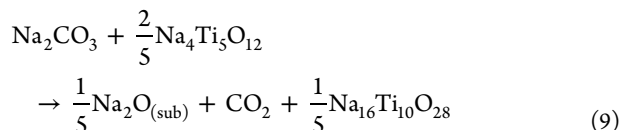
formation could be explained by two different mechanisms. (1) If the quantity of sodium released from  $\text{Na}_2\text{TiO}_3$  is reduced more than that observed at around 600–650 °C, the following reactions 7 and 8 may be established.



where  $\text{Na}_2\text{CO}_3$  decomposes immediately, as follows:



(2) On the contrary, if reaction 2 prevails, part of the sodium must sublime as  $\text{Na}_2\text{O}$  during  $\text{CO}_2$  desorption, while the other part of the sodium atoms must be reincorporated to the  $\text{Na}_4\text{Ti}_5\text{O}_{12}$  structure (reaction 9). In any case,  $\text{Na}_2\text{O}$  sublimation is proposed (reaction 8) based on the fact that  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$  possesses a more similar density (2.05 g/cm<sup>3</sup>) than does  $\text{Na}_4\text{Ti}_5\text{O}_{12}$ , which may have inhibited the  $\text{Na}_2\text{TiO}_3$  total regeneration. It is confirmed as the final weight decreased more than 100 wt %, on those isotherms.



The morphology evolution of the  $\text{Na}_2\text{TiO}_3$ – $\text{CO}_2$  system was followed by SEM. Figure 8 shows the backscattered images of the  $\text{Na}_2\text{TiO}_3$  sample, for comparison purposes, and the  $\text{Na}_2\text{TiO}_3$ – $\text{CO}_2$  isothermal products obtained at 400, 600, and 750 °C. As it was previously described, the  $\text{Na}_2\text{TiO}_3$  and the isothermal product of 400 °C presented similar particle sizes and shapes (Figure 8A,B). In fact, the only difference between these two samples was the superficial formation of the  $\text{Na}_2\text{O}$  spherical particles. However, the morphology varied significantly when the isotherm was performed at 600 °C. At this temperature, two different particles can be observed, some being flake-like particles surrounded by a dense matrix (Figure 8C). The presence of two different phases was determined by the particle contrasts observed in the corresponding back scattered electron images (BSEI), and they must correspond to  $\text{Na}_2\text{CO}_3$  and  $\text{Na}_4\text{Ti}_5\text{O}_{12}$ , because they were the  $\text{Na}_2\text{TiO}_3$  carbonation products detected by XRD. Thus, the contrast differences arise from the differences in mean atomic number ( $\bar{Z}$ ) of  $\text{Na}_2\text{CO}_3$  and  $\text{Na}_4\text{Ti}_5\text{O}_{12}$ , 8.666 and 11.904, respectively. Therefore, the back scattered electron coefficient ( $\eta$ ) of these phases increases from 0.0999 to 0.1144 for  $\text{Na}_2\text{CO}_3$  (dark phase) and  $\text{Na}_4\text{Ti}_5\text{O}_{12}$  (light phase), respectively. Finally, the morphology of the 750 °C isothermal product ( $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$ ) presented very dense agglomerates composed of polyhedral particles of around 0.5–2  $\mu\text{m}$  (Figure 8D). This morphology must have evolved from the original  $\text{Na}_2\text{TiO}_3$  particles, which partially reacted with  $\text{CO}_2$  producing  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$ , sublimating  $\text{Na}_2\text{O}$ , but mainly sintering.

Figures 9 and 10 show the calculated thermodynamic properties of  $\text{CO}_2$  capture reactions by these sodium titanates. For comparison, the properties of  $\text{Na}_2\text{ZrO}_3$  capture  $\text{CO}_2$  are also presented in the same figures. It can be seen that there is a discrepancy between the  $\text{Na}_2\text{TiO}_3$  calculated data reported here and the previously reported values fitted from HSC Chemistry database.<sup>95</sup> The differences arise from the initial structures used in each case. While the HSC reported value was measured with a  $\text{Na}_2\text{O}$ – $\text{TiO}_2$  mixture, the calculations in the present work were performed on the perfect crystal structure (*Immm*). In the

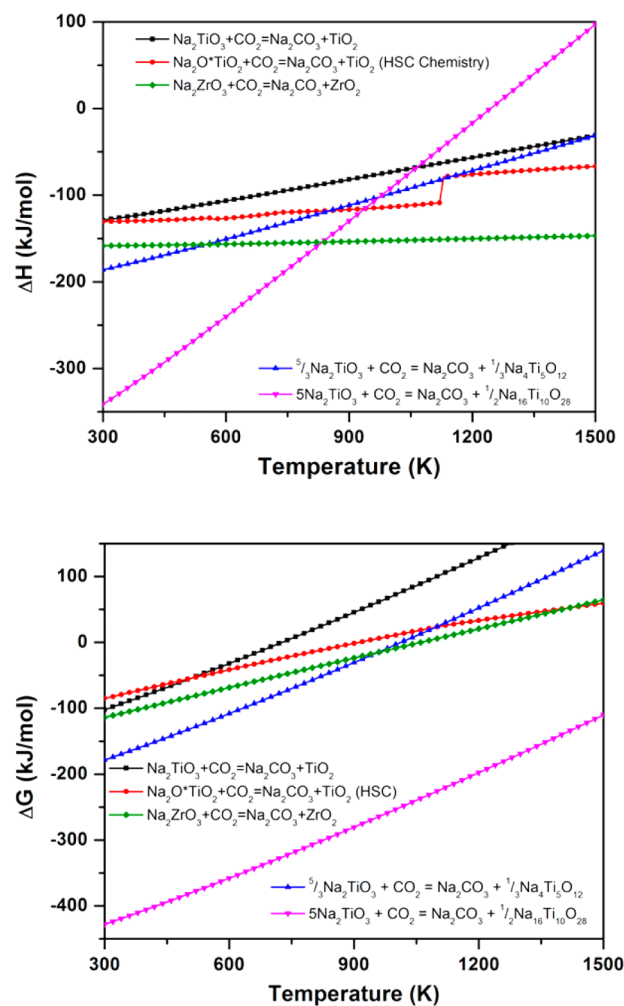


Figure 9. Calculated thermodynamic properties of  $\text{CO}_2$  capture reactions by different sodium titanates and sodium zirconate.

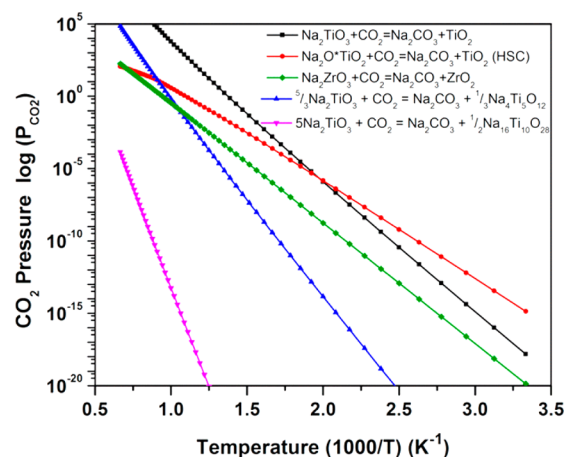


Figure 10. Calculated van't Hoff plots for reactions of sodium titanates and zirconate with  $\text{CO}_2$ .

phonon calculations, there are a few soft modes (negative frequency) which may cause some errors in evaluating thermodynamic properties and indicate phase deformation/change. As shown in Figure 9, when  $\text{Na}_2\text{TiO}_3$  captures  $\text{CO}_2$ , producing  $\text{TiO}_2$ -rich sodium titanates ( $\text{Na}_4\text{Ti}_5\text{O}_{12}$  and  $\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$ ), the corresponding heat of reaction ( $\Delta H$ ) and

**Table 2.** Theoretical Weight Percentage of CO<sub>2</sub> Capture, The Energy Change ( $\Delta E_{\text{DFT}}$ ), and the Thermodynamic Properties ( $\Delta H$ ,  $\Delta G$ , at  $T = 300$  K)<sup>a</sup>

reaction	CO <sub>2</sub> absorbed (wt %)	$\Delta E_{\text{DFT}}$ (kJ/mol)	$\Delta H$ (T = 300 K) (kJ/mol)	$\Delta G$ (T = 300 K) (kJ/mol)	$T_1$ (K)	$T_2$ (K)	$T_3$ (K)
$\text{Na}_2\text{TiO}_3 + \text{CO}_2 = \text{Na}_2\text{CO}_3 + \text{TiO}_2$	31.24	-158.418	-128.917 (-130.367) <sup>b</sup>	-102.385 (-85.359) <sup>b</sup>	680	810	740
$5/3\text{Na}_2\text{TiO}_3 + \text{CO}_2 = \text{Na}_2\text{CO}_3 + 1/3\text{Na}_4\text{Ti}_5\text{O}_{12}$	18.74	-234.443	-186.046	-178.411	945	1120	1020
$5\text{Na}_2\text{TiO}_3 + \text{CO}_2 = \text{Na}_2\text{CO}_3 + 1/2\text{Na}_{16}\text{Ti}_{10}\text{O}_{28}$	6.25	-484.413	-341.321	-391.401	hT <sup>c</sup>	hT	hT
$\text{Na}_2\text{O}_{(\text{sub})} + \text{CO}_2 = \text{Na}_2\text{CO}_3$ <sup>d</sup>	70.99	-284.707	-282.372	-231.900	hT	hT	hT
$1/5\text{Na}_2\text{O}_{(\text{sub})} + \text{CO}_2 + 1/5\text{Na}_{16}\text{Ti}_{10}\text{O}_{28} = \text{Na}_2\text{CO}_3 + 2/5\text{Na}_4\text{Ti}_5\text{O}_{12}$	16.22	-418.155	-303.309	-324.274	hT	hT	hT
$\text{Na}_2\text{ZrO}_3 + \text{CO}_2 = \text{Na}_2\text{CO}_3 + \text{ZrO}_2$ <sup>e</sup>	23.76	-140.684	-158.327	-114.121	925	1275	1065

<sup>a</sup>The turnover temperatures ( $T_1$ ,  $T_2$ ,  $T_3$ ) of these CO<sub>2</sub> capture reactions under the conditions of post-combustion ( $P_{\text{CO}_2} = 0.1$  bar), pre-combustion ( $P_{\text{CO}_2} = 20$  bar), and  $P_{\text{CO}_2} = 1$  bar are also listed. <sup>b</sup>From HSC Chemistry database 95. <sup>c</sup>hT means the temperature exceeds our temperature range (1500 K). <sup>d</sup>From ref 99. <sup>e</sup>From ref 98.

Gibbs free ( $\Delta G$ ) energies become more negative, resulting in higher turnover temperatures (Figure 10). However, the theoretical CO<sub>2</sub> capacity is reduced as it is summarized in Table 2.

To further analyze the isothermal curves presented in Figure 5, these data were fitted to a first-order reaction.<sup>30,65,70</sup> This model was selected as there are several processes involved in this reaction-mechanism, thus it was not possible to fit the data to multiple exponential models. However, during the first moments of the CO<sub>2</sub> chemisorption process, one can assume that a first-order reaction is taking place with respect to Na<sub>2</sub>TiO<sub>3</sub> surface particles, as CO<sub>2</sub> was present in excess (60 mL/min). Therefore, the rate law can be assumed as follows:

$$\ln[\text{Na}_2\text{TiO}_3] = -kt \quad (10)$$

in which  $k$  is the reaction rate constant,  $t$  is the time, and  $[\text{Na}_2\text{TiO}_3]$  is the molar concentration of the ceramic. As expected, data trends were linear only over very short intervals (60 s approximately), assuming a superficial Na<sub>2</sub>TiO<sub>3</sub> carbonation reaction, and before any diffusion process or Na<sub>2</sub>TiO<sub>3</sub> structural change are produced. The corresponding  $k$  values are presented in Table 3.  $k$  values tend to increase as a

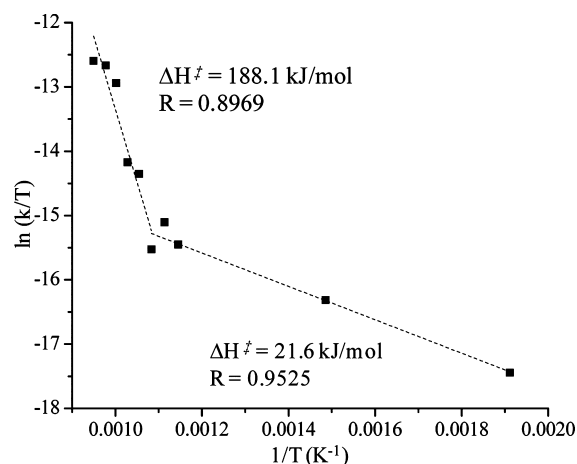
**Table 3.** First-Order Reaction Rate Constants of the Na<sub>2</sub>TiO<sub>3</sub>-CO<sub>2</sub> System at Different Temperatures

temperature (°C)	$k$ (seg <sup>-1</sup> )
250	$1.38 \times 10^{-5}$
400	$5.53 \times 10^{-5}$
600	$1.70 \times 10^{-4}$
625	$2.48 \times 10^{-4}$
650	$1.67 \times 10^{-4}$
675	$5.55 \times 10^{-4}$
700	$6.82 \times 10^{-4}$
725	$2.40 \times 10^{-3}$
750	$3.23 \times 10^{-3}$
780	$3.57 \times 10^{-3}$

function of temperature. In addition, if these kinetic data are compared to similar  $k$  values, obtained for other alkaline ceramics, it can be seen that these values are lower than those reported for the Li<sub>8</sub>SiO<sub>6</sub> and Na<sub>2</sub>ZrO<sub>3</sub>, among others.<sup>30,70,74-76</sup> Specifically, Na<sub>2</sub>ZrO<sub>3</sub><sup>70,74-76</sup> reported  $k$  values between  $1 \times 10^{-3}$  and  $2 \times 10^{-2}$  s<sup>-1</sup> at the optimum temperatures (600–700 °C), while the  $k$  values obtained with Na<sub>2</sub>TiO<sub>3</sub>, between 600 and 650 °C (the optimum temperature range), were around  $1.7$  and  $2.5 \times 10^{-4}$  s<sup>-1</sup>. Thus, these results clearly show that CO<sub>2</sub>

chemisorption on Na<sub>2</sub>TiO<sub>3</sub> is slower than that on Na<sub>2</sub>ZrO<sub>3</sub>, although both sodium ceramics possess similar crystalline layered structures. This important difference may be related to variations observed on the structural evolution of each ceramic. While Na<sub>2</sub>ZrO<sub>3</sub> evolves directly to Na<sub>2</sub>CO<sub>3</sub> and ZrO<sub>2</sub>, Na<sub>2</sub>TiO<sub>3</sub> reacts only partially to produce Na<sub>2</sub>CO<sub>3</sub> and different sodium titanates with lower Na:Zr molar ratios. So, sodium reactivity seems to be more limited on sodium titanate.

From Figure 10, a comparison of Na<sub>2</sub>TiO<sub>3</sub> with Na<sub>2</sub>ZrO<sub>3</sub> shows that, under the same CO<sub>2</sub> pressure, the turnover temperature for Na<sub>2</sub>TiO<sub>3</sub> capturing CO<sub>2</sub> is lower than that of Na<sub>2</sub>ZrO<sub>3</sub>, as the latter reacting with CO<sub>2</sub> has more negative heat of reaction and Gibbs free energy with increasing temperatures. Likewise, if  $k$  values are dependent on temperature, the plot of  $\ln k/T$  versus  $1/T$  should produce a straight line according to Eyring's model, which is used for heterogeneous reactions (Figure 11) and allows a determi-

**Figure 11.** Eyring-type plot of  $\ln k/T$  vs  $1/T$  for data obtained assuming a first-order reaction of  $[\text{Na}_2\text{TiO}_3]$  into a saturated CO<sub>2</sub> flux. Only the data obtained between 600 and 780 °C was considered for this analysis.

nation of the activation enthalpy ( $\Delta H^\ddagger$ ). In the Na<sub>2</sub>TiO<sub>3</sub>-CO<sub>2</sub> system, two different  $\Delta H^\ddagger$  trends were determined. Between 200 and 650 °C the  $\Delta H^\ddagger$  value was 21.6 kJ/mol, while at higher temperatures (650–780 °C), it was equal to 188.1 kJ/mol. These results indicate that the CO<sub>2</sub> chemisorption in Na<sub>2</sub>TiO<sub>3</sub> has a higher temperature dependence than those determined from other alkaline ceramics, such as Na<sub>2</sub>ZrO<sub>3</sub> (33 kJ/mol).<sup>75</sup> It



means that CO<sub>2</sub> chemisorption on Na<sub>2</sub>TiO<sub>3</sub> is highly dependent on temperature.

From all these results, it can be established that CO<sub>2</sub> chemisorption on Na<sub>2</sub>TiO<sub>3</sub> depends on different factors. Although CO<sub>2</sub> reacts with the Na<sub>2</sub>TiO<sub>3</sub> particle surfaces as a function of temperature (kinetics results), the Na<sub>2</sub>TiO<sub>3</sub> structural evolution seems to control the sodium accessibility and consequently the CO<sub>2</sub> chemisorption–desorption equilibrium. Sodium atoms seem to be partially extracted from the layered Na<sub>2</sub>TiO<sub>3</sub> crystalline structure to react with CO<sub>2</sub>, producing Na<sub>2</sub>CO<sub>3</sub> and Na<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> or Na<sub>16</sub>Ti<sub>10</sub>O<sub>28</sub> depending on temperature.

#### IV. CONCLUSIONS

Na<sub>2</sub>TiO<sub>3</sub> was synthesized via a solid state reaction. The sample structure and microstructure were analyzed using XRD, SEM, TEM, and N<sub>2</sub> adsorption. The CO<sub>2</sub> chemisorption capacity on Na<sub>2</sub>TiO<sub>3</sub> was evaluated both dynamically and isothermally thermogravimetrically, in which the isothermal products were recharacterized using XRD, SEM, and TEM. Between 250 and 400 °C, CO<sub>2</sub> is initially chemisorbed on Na<sub>2</sub>TiO<sub>3</sub>, which must produce Na<sub>2</sub>CO<sub>3</sub>. However, CO<sub>2</sub> is desorbed after some minutes, leaving the sodium atoms as Na<sub>2</sub>O (determined by XRD and TEM) over the Na<sub>2</sub>TiO<sub>3</sub> particle surfaces. As the temperature is not very high, sodium seems not to be kinetically able to be reincorporated into the Na<sub>2</sub>TiO<sub>3</sub> structure. Then, at higher temperatures (600–650 °C), the CO<sub>2</sub> chemisorption evolved to form different phases, Na<sub>2</sub>CO<sub>3</sub> (produced due to the CO<sub>2</sub> chemisorption) and Na<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>, in addition to Na<sub>2</sub>O. Thus, the Na<sub>2</sub>O formation may be related to a partial CO<sub>2</sub> desorption process. However, at  $T \geq 650$  °C Na<sub>2</sub>CO<sub>3</sub>, Na<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>, and Na<sub>2</sub>O tended to disappear, while Na<sub>16</sub>Ti<sub>10</sub>O<sub>28</sub> is formed. In fact, Na<sub>16</sub>Ti<sub>10</sub>O<sub>28</sub> was the only phase detected at 780 °C.

The kinetic parameter values ( $k$ ) obtained for the Na<sub>2</sub>TiO<sub>3</sub>–CO<sub>2</sub> reaction mechanism tend to increase as a function of temperature. In addition, the  $\Delta H^\ddagger$  value is 140.9 kJ/mol between 600 and 780 °C. It means that CO<sub>2</sub> chemisorption on Na<sub>2</sub>TiO<sub>3</sub> is highly dependent on temperature.

These results revealed that CO<sub>2</sub> chemisorption on Na<sub>2</sub>TiO<sub>3</sub> depends on different factors. The Na<sub>2</sub>TiO<sub>3</sub> structural evolution seems to be controlled by the sodium accessibility and consequently by the CO<sub>2</sub> chemisorption–desorption equilibrium. In fact at low temperatures Na<sub>2</sub>O is produced due to an incomplete CO<sub>2</sub> chemisorption process. Later at higher temperatures Na<sub>2</sub>TiO<sub>3</sub> reacts with CO<sub>2</sub> to produce Na<sub>2</sub>CO<sub>3</sub> and Na<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> or Na<sub>16</sub>Ti<sub>10</sub>O<sub>28</sub> depending on the temperature range.

Additionally, all previous results were corroborated based on the theoretical thermodynamic data for the Na<sub>2</sub>TiO<sub>3</sub>–CO<sub>2</sub> reaction system, where different reaction products were estimated (TiO<sub>2</sub>, Na<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>, or Na<sub>16</sub>Ti<sub>10</sub>O<sub>28</sub>).  $\Delta E_{\text{DFT}}$ ,  $\Delta H$ , and  $\Delta G$  values clearly showed the different thermal stability of each reaction process at different temperature ranges.

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##### Notes

The authors declare no competing financial interest.

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