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Separation of CO₂ from CH₄ and CO₂ capture in the presence of water vapour in NOTT-400†

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Maximiliano R. Gonzalez,^a Juan H. González-Estefan,^b Hugo A. Lara-García,^b
Pedro Sánchez-Camacho,^b Elena I. Basaldella,^{ac} Heriberto Pfeiffer^b and
Ilich A. Ibarra^{*b}

From a binary equimolar gas-mixture of CO₂ and CH₄, NOTT-400 shows CO₂ separation from CH₄. By kinetic uptake experiments, this material confirms a maximum of 4.3 wt% CO₂ capture at 30 °C and a significant 2-fold increase (~9.3 wt%) in CO₂ capture under 40% relative humidity of water vapour.

Air pollution and global warming are two of the foremost threats to our civilisation.^{1–6} Of particular significance are the rapidly increasing levels of carbon dioxide (CO₂) emissions, due to burning of fossil fuels. Fossil fuels are non-renewable⁷ and cannot continue as a principal energy source in the far future⁸ due to the limited reserves. Natural gas (CH₄) is a very desirable fuel because it burns cleaner than any other fossil fuel (*e.g.* petrol or coal).⁹ However, the quality of natural gas, coming from land fields and biogas plants, is considerably low with impurities like CO₂ (20 to 35%), N₂, H₂O and H₂S.¹⁰ Then, pre-combustion CO₂ capture from natural gas is essential to maximise its energy content. Additionally, post-combustion CO₂ capture from plant flue gas is also crucial in order to control greenhouse emissions.¹¹

CO₂ separation and sequestration have extremely motivated many governments to invest in the development of new methods for efficiently and effectively capturing CO₂.¹² Conventional adsorption in aqueous alkanolamine solutions has been extensively used and studied, but they have many major limitations as adsorbents for industrial CO₂ capture due to their heat instability and corrosion towards vessels and pipelines.¹³ Thus, the use of porous solids for the adsorption of CO₂ is a timely research area and the search for materials with a high adsorption capacity, structural stability,

fast sorption kinetics and mild regeneration properties remains a major challenge.

Porous coordination polymers (PCPs) or metal–organic frameworks (MOFs) are amongst the most promising candidates for gas separation, because their sorption selectivity towards small molecule adsorbates is directly tunable as a function of the topology and chemical composition of the micropores.^{14,15} Despite the high CO₂ capacity and selectivity that PCPs show, many gas separation processes involve the exposure to water vapour. However, few PCPs have shown good stability to water, and water is most often unfavourable to gas separations.¹⁶ Among those few examples, Hong *et al.*¹⁷ reported a water-stable PCP based on a binuclear [In₂(μ₂-OH)] building block (see Scheme S1, ESI†), InOF-1, constructed from a flexible BPTC⁴⁻ ligand (H₄BPTC = biphenyl-3,3',5,5'-tetracarboxylic acid) which also showed high CO₂/N₂ and CO₂/CH₄ selectivities (by using the experimental single-component gas adsorption isotherms). Interestingly, the effect of water on the CO₂ capture has only recently been investigated on PCPs.^{18,19}

Llewellyn and co-workers²⁰ investigated the CO₂ adsorption in some PCPs under different relative humidities of water vapour. Indeed, HKUST-1 was shown to degrade in the presence of humidity, and UiO-66 did not show any enhanced CO₂ uptake.²⁰ In the case of MIL-100(Fe), a remarkable 5-fold increase in CO₂ uptake was observed with increasing relative humidity (RH), 105 mg g⁻¹ at 40% RH. Additionally, Yaghi *et al.*²¹ showed that the presence of hydroxyl functional groups increases the affinity of the framework for water. Thus, in the present work we have chosen a material entitled NOTT-400²² based on a binuclear [Sc₂(μ₂-OH)] building block (see Scheme S1, ESI†) which is isostructural to the water-stable InOF-1¹⁷ and possesses hydroxo functional groups (μ₂-OH) to study the separation of a binary gas mixture (not a single-component gas) of CO₂ and CH₄ and we have successfully performed CO₂ capture in the presence of water vapour.

After the first gas separation experiment was carried out (see Experimental), the most characteristic FTIR bands for the CO₂ (2349 cm⁻¹) and CH₄ (3016 cm⁻¹) molecules were analysed. In Fig. 1 it is possible to observe a continuous increase in the

^a Centro de Investigación y Desarrollo en Ciencias Aplicadas Dr. J. J. Ronco (CINDECA), (CONICET-CIC-UNLP) 47 No. 257, (B1900 AJK) La Plata, Argentina

^b Instituto de Investigaciones en Materiales, Universidad Nacional Autónoma de México, Circuito Exterior s/n, CU, Del. Coyoacán, 04510, México D. F., Mexico.

E-mail: argel@unam.mx

^c CITEMA, Universidad Tecnológica Nacional, 60 y 124, (1900) La Plata, Argentina

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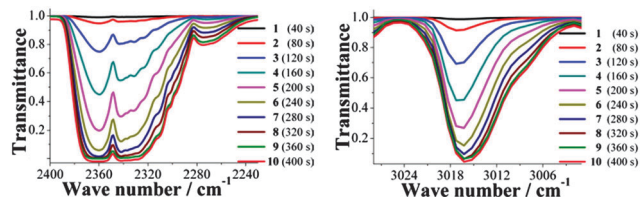


Fig. 1 FTIR spectra of the resulting exit exhaust of the binary equimolar ($0.13 \text{ mmol min}^{-1}$) gas-mixture of CO_2 and CH_4 : (left) the characteristic CO_2 band and (right) the characteristic CH_4 band.

characteristic band intensities (Fig. 1) for CO_2 and CH_4 with time. In other words, from spectrum 1 to spectrum 10 the intensity of the characteristic FTIR band increases while the transmittance decreases.

The intensities of these characteristic FTIR bands (for CO_2 and CH_4) were shown to be different. This could suggest that the CO_2 and CH_4 molecules arrive at the FTIR detector with different times. By normalising the intensities, considering their respective transmittances, it is possible to plot the increase in intensity of each scan for CO_2 and CH_4 simultaneously (Fig. 2, left). For each scan, the normalised intensity of CH_4 is higher than CO_2 , suggesting that the molecules of CH_4 effectively arrive at the FTIR detector before the CO_2 molecules. We can rationalise this result as follows: when the binary gas mixture (CO_2 and CH_4) flows through the activated sample NOTT-400 this material retains CO_2 stronger than CH_4 , and therefore, the CH_4 gas molecules flow 'faster' inside the material and are detected earlier. In order to confirm this hypothesis, we carried out three more experiments: first, an acetone-exchanged sample of NOTT-400 (40 mg) was placed into the BEL-REA system, activated and stabilised as described (*vide supra*) and a flow of only CO_2 gas ($0.13 \text{ mmol min}^{-1}$) was set. Then, the resulting flow gas was analysed by FTIR spectroscopy and 10 scans were recorded, until the detector was saturated (see Fig. S5, ESI[†]). Second, another acetone-exchanged NOTT-400 (40 mg) sample was mounted in the BEL-REA system, activated, stabilised and analysed as described earlier. This time, the sample was exposed to a flow of only CH_4 gas ($0.13 \text{ mmol min}^{-1}$). As in the previous experiment, 10 FTIR spectra were collected from the resulting flow gas until the detector was saturated (see Fig. S6, ESI[†]). Again, by normalising the characteristic FTIR intensities it was possible to simultaneously plot the normalised intensity of each scan for CO_2 and CH_4 (Fig. 2, right).

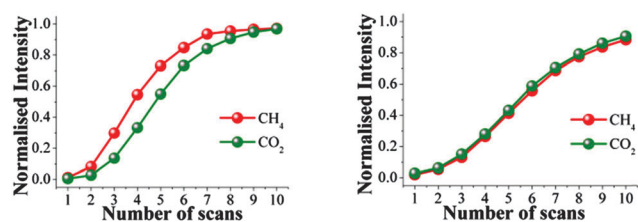


Fig. 2 Normalised characteristic FTIR intensities of CO_2 and CH_4 as a function of the number of scans. (left) FTIR intensities from a resulting exit exhaust of the binary equimolar ($0.13 \text{ mmol min}^{-1}$) gas-mixture of CO_2 and CH_4 ; (right) FTIR intensities from individual flows of CO_2 and CH_4 .

Thus, the normalised intensities for CO_2 and CH_4 at each scan (from 1 to 10) are practically the same (Fig. 2, right) suggesting that when the resulting flow of each pure-gas component (not a mixture of gases) is analysed separately by FTIR spectroscopy, the molecules of CO_2 and CH_4 arrive at the same time to the FTIR detector. These results confirm that NOTT-400 is more selective to CO_2 than CH_4 when a binary equimolar ($0.13 \text{ mmol min}^{-1}$) gas-mixture of CO_2 and CH_4 flows through an activated sample. We interpreted this selectivity as the time delay of the CO_2 molecules in reaching the FTIR detector. By polynomial regressions of the normalised intensities in Fig. 2 (left), we estimated this delay to be $\sim 28 \text{ s}$ (see Fig. S7 and S8, ESI[†]). Finally a third experiment was carried out: in order to confirm that this delay was caused by the adsorption selectivity shown by NOTT-400 (a microporous PCP) rather than other phenomena, a non-porous material was mounted in the BEL-REA system. PCM-14²³ is a dense coordination polymer that has shown to be a non-porous material when it is activated between $25\text{--}150 \text{ }^\circ\text{C}$. Thus, a sample of PCM-14 (40 mg) was activated at $150 \text{ }^\circ\text{C}$ for 2 h under a flow of N_2 gas and then directly exposed to a binary equimolar ($0.13 \text{ mmol min}^{-1}$) CO_2 and CH_4 gas mixture. Thus, the resulting flow gas was analysed by FTIR spectroscopy and just 6 scans were recorded, until the detector was saturated. By normalisation of the characteristic FTIR intensities, we plotted the normalised intensities of each CO_2 and CH_4 scan (see Fig. S9, ESI[†]). Interestingly, the normalised intensities for CO_2 and CH_4 at each scan (from 1 to 6) are practically the same (see Fig. S9, ESI[†]) confirming that the time delay is due to the microporosity of NOTT-400.

Dynamic and isothermal CO_2 experiments were carried out on NOTT-400 (see Experimental thermobalance, ESI[†]). Fig. 3, left, shows the kinetic uptake experiments from $30 \text{ }^\circ\text{C}$ to $100 \text{ }^\circ\text{C}$. At $30 \text{ }^\circ\text{C}$ the material exhibited the maximum weight% gain, which represents the maximum amount of CO_2 captured.

This amount corresponds to 4.3 wt% and it was rapidly reached after just $\sim 300 \text{ s}$ (5 min) and it remained constant until the end of the experiment (3600 s or 60 min). At $40 \text{ }^\circ\text{C}$ the uptake was estimated to be 3.5 wt% and it was also reached after around 300 s (Fig. 3, left). Clearly, while the temperature is increased (from 30 to $100 \text{ }^\circ\text{C}$), the CO_2 weight(%) decreases gradually (Fig. 3, left) to 0.5 wt% (at $100 \text{ }^\circ\text{C}$). In order to confirm that this decrease is not due to sample degradation, we have run PXRD measurements on each sample after these CO_2 capture experiments. Fig. 3 (right)

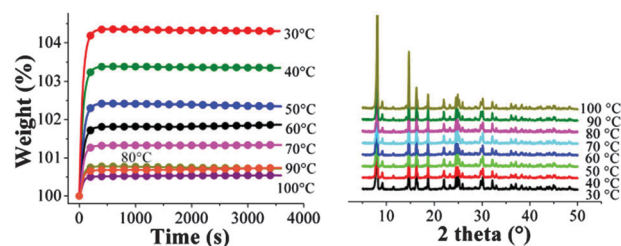


Fig. 3 (left) Kinetic uptake experiments performed at different temperatures ($30, 40, 50, 60, 70, 80, 90$ and $100 \text{ }^\circ\text{C}$) with a CO_2 flow of 60 mL min^{-1} . Each curve shows the experimental data and the symbols were used to differentiate them; (right) PXRD patterns of each NOTT-400 sample after the kinetic CO_2 isotherms were carried out at different temperatures.

shows that the crystallinity of the samples after each CO₂ capture experiment was retained. Indeed, we increased the temperature progressively up to 650 °C (see Fig. S10, ESI†) and there is a constant weight loss, suggesting that samples of activated NOTT-400 are not capturing CO₂ after 150 °C and what we observe is a gradual structural decomposition which was confirmed by PXRD (see Fig. S10, ESI†).

Motivated by the very promising results that Hong *et al.* reported,¹⁷ by showing an isostructural framework to NOTT-400 (InOF-1), which is water stable and exhibited high CO₂/N₂ and CO₂/CH₄ selectivities, we explored the water stability of NOTT-400. Then, acetone-exchanged samples of NOTT-400 were exposed to air and soaked in distilled water. PXRD patterns of these experiments (see Fig. S11, ESI†) then confirmed the structural stability of NOTT-400 in water. This water-stability can be attributed to the presence of the hydroxo functional groups (within the pores of NOTT-400) which has been previously shown²¹ and these functional groups enhance the affinity of the material for water. Thus, after establishing the best CO₂ capture temperature (30 °C, Fig. 3, left), a kinetic isotherm experiment at 30 °C, with a constant CO₂ flow and a relative humidity (RH) of 40%, was carried out. It was decided to run this experiment with a 40% RH based on the remarkable results that Llewellyn *et al.*²⁰ previously reported (5-fold increase in CO₂ uptake for MIL-100(Fe)).

An activated NOTT-400 sample (150 °C for 2 h and under a flow of N₂ gas) was placed into a humidity-controlled thermobalance. After activation of the material, the equipment was stabilised at 40% RH (30 °C) and a constant CO₂ flow (60 mL min⁻¹) was started. Later, we repeated this experimental procedure on a different activated NOTT-400 sample and set a constant N₂ flow (60 mL min⁻¹). Fig. 4 shows the kinetic uptake experiments at 30 °C and 40% RH for CO₂ and N₂. For both isotherms, it is clearly observed that the material shows a constant increase in weight (while the experiment is progressing with time, see Fig. 4). This increase in weight is due the contribution of water and CO₂ or water and N₂, respectively.

In order to find the maximum CO₂ capture under 40% RH conditions, we need to differentiate the contribution of water to the weight increase. By simply taking the difference of the two isotherms (CO₂ and N₂) we could obtain the CO₂ capture at 40% RH. This is valid if the material does not capture any N₂ at 30 °C. Therefore, by performing a kinetic uptake experiment on an activated NOTT-400 sample at 30 °C without any presence of water vapour (0% RH) with a constant N₂ flow (60 mL min⁻¹)

we obtained a N₂ capture of approximately 0.01 wt%. This result is consistent with previous reports where the capacity of N₂ capture in PCPs at room temperatures is basically negligible.²⁴ In Fig. 4, the gradual weight increase (for CO₂/H₂O and N₂/H₂O) starts at 0 s and stabilises at ~6000 s (100 min). Interestingly, under anhydrous conditions the CO₂ uptake rapidly reached stability (5 min, see Fig. 3, left). This equilibrium discrepancy is due to the nature of the vapour adsorption process that in general takes considerably more time to reach stability than the gas adsorption process in microporous materials.²⁵ Then, from 600 s until approximately 11 000 s (183.3 min) both isotherms seem to reach a plateau where both uptakes are practically constant. At 11 000 s, the maximum amounts of CO₂/H₂O and N₂/H₂O captured are 51.1 wt% and 41.8 wt%, respectively and by taking the difference of these two values (since there is no N₂ uptake at 30 °C) the CO₂ capture in the materials is ~ 9.3 wt%. Finally, from 11 000 s to 13 000 s (Fig. 4, red rectangle) the flow of each gas and the relative humidity were stopped and the decrease in weight represents the gas and water vapour desorption. Therefore, the CO₂ capture was approximately 2-fold increased with a 40% RH. This enhancement in CO₂ uptake in the presence of water can be explained by CO₂ confinement effects induced by bulky molecules (H₂O).²⁶ Additionally, we decided to run a CO₂ experiment (60 mL min⁻¹) at 40% RH and 30 °C on an activated PCM-14²³ sample (150 °C for 2 h, under a flow of N₂ gas). Since PCM-14 is a non-porous material, when activated between 25–150 °C, it provided a direct CO₂ capture comparison to NOTT-400 (microporous material). Thus, from 0 s to 11 000 s the maximum CO₂ uptake (under 40% RH) was 0.8 wt% (see Fig. S12, ESI†). This result corroborated that there is no CO₂ sequestration in a non-porous material when the relative humidity is 40% at 30 °C.

In summary, the Sc(III) coordination polymer NOTT-400 shows CO₂ separation from CH₄, in a more realistic scenario, when this material was exposed to a binary, CO₂/CH₄, equimolar gas-mixture. By kinetic isotherm experiments, NOTT-400 exhibits a total CO₂ amount of 4.3 wt% at 30 °C, which was rapidly reached after just approximately 300 s. Additionally, NOTT-400 exhibits high stability towards humidity, which was confirmed by PXRD. Due to this particularly high stability, NOTT-400 performs CO₂ uptake under relative humidity conditions (40% RH) and 30 °C, displaying a maximum CO₂ capture of approximately 9.3 wt%.

Experimental

Gas separation experiments

A catalytic reactor system (BEL-REA, BEL Japan; Fig. S3, ESI†) was employed, which allowed each sample of acetone-exchanged NOTT-400 (see Experimental, ESI†) to be activated (150 °C for 2 h) under a flow of N₂ gas and then directly exposed to adsorbates (CO₂ and CH₄) *in situ*, and studied by FTIR spectroscopy over many cycles without physical manipulation or exposure to air. In each study, an acetone-exchanged sample of NOTT-400 (40 mg) was placed into the holder sample in the BEL-REA system and activated as described above. Then, the system was allowed to cool down to 30 °C and the activated sample was exposed to a

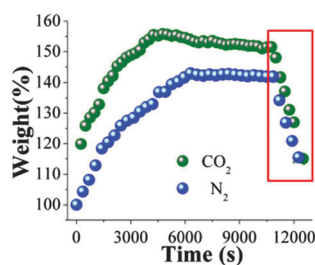


Fig. 4 Kinetic uptake experiments carried out at 30 °C and 40% RH with CO₂ (green spheres) and N₂ (blue spheres) flows of 60 mL min⁻¹, respectively.

flow of the binary equimolar ($0.13 \text{ mmol min}^{-1}$) gas mixture of CO_2 and CH_4 . This mixture represents a more realistic composition for gas separation processes. Next, after stabilisation of the gas flow within the sample, the resulting exit exhaust gases (see Fig. S3, ESI[†]) was analysed by FTIR spectroscopy. Thus, each FTIR spectrum was recorded every 40 seconds ($\sim 0.66 \text{ min}$), until the detector was saturated, to make a total of 10 FTIR spectra (see Fig. S4, ESI[†]).

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Notes and references

- 1 F. W. Lipfert, *Air Pollution and Community Health: A Critical Review and Data Source Book*, Van Nostrand Reinhold, New York, USA, 1994, p. 556.
- 2 P. D. Noyes, M. K. McElwee, H. D. Miller, B. W. Clark, L. A. Van Tiem, K. C. Walcott, K. N. Erwin and E. D. Levin, *Environ. Int.*, 2010, **35**, 971.
- 3 J. F. Zhang and K. R. Smith, *Br. Med. Bull.*, 2003, **68**, 209.
- 4 J. T. Litynski, S. M. Klara, H. G. McIlvried and R. D. Srivastava, *Environ. Int.*, 2006, **32**, 128.
- 5 M. Z. Jacobson, *Energy Environ. Sci.*, 2009, **2**, 148.
- 6 International Energy Agency (IEA), *Key World Energy Statistics*, OECD/IEA, France, 2013.
- 7 M. Z. Jacobson, *Geochim. Cosmochim. Acta*, 2009, **73**, A581.
- 8 A. Züttel, A. Borgschulte and L. Schlapbach, *Hydrogen as a Future Energy Carrier*, Wiley-VCH, Weinheim, Germany, 2008, p. 441.
- 9 T. Burchell and M. Rogers, *SAE Tech. Pap. Ser.*, 2000, 2000.
- 10 M. Herout, J. Malat'ák, L. Kučera and T. Dlabaja, *Res. Agric. Eng.*, 2011, **57**, 137.
- 11 D. M. D'Alessandro, B. Smit and J. R. Long, *Angew. Chem., Int. Ed.*, 2010, **49**, 6058.
- 12 K. Sumida, D. L. Rogow, J. A. Mason, T. M. McDonald, E. D. Bloch, Z. R. Herm, Z. T.-H. Bae and J. R. Long, *Chem. Rev.*, 2012, **112**, 724.
- 13 (a) G. T. Rochelle, *Science*, 2009, **325**, 1652; (b) F. Karadas, M. Atilhan and S. Aparicio, *Energy Fuels*, 2010, **24**, 5817.
- 14 (a) S. Yang, G. S. B. Martin, G. J. J. Titman, A. J. Blake, D. R. Allan, N. R. Champness and M. Schröder, *Inorg. Chem.*, 2011, **50**, 9374; (b) A. J. Nuñez, L. N. Shear, N. Dahal, I. A. Ibarra, J. W. Yoon, Y. K. Hwang, J.-S. Chang and S. M. Humphrey, *Chem. Commun.*, 2011, **47**, 11855.
- 15 (a) H. Furukawa, N. Ko, Y. B. Go, N. Aratani, S. B. Choi, E. Choi, A. Ö. Yazaydin, R. Q. Snurr, M. O'Keeffe, J. Kim and O. M. Yaghi, *Science*, 2010, **329**, 424; (b) A. M. Bohnsack, I. A. Ibarra, P. W. Hatfield, J. W. Yoon, Y. K. Hwang, J.-S. Chang and S. M. Humphrey, *Chem. Commun.*, 2011, **47**, 4899; (c) P. Nugent, Y. Belmabkhout, S. D. Burd, A. J. Cairns, R. Luebke, K. Forrest, T. Pham, S. Ma, B. Space, L. Wojtas, M. Eddaoudi and M. J. Zaworotko, *Nature*, 2013, **495**, 80.
- 16 (a) S. S. Nagarkar, A. K. Chaudhari and S. K. Ghosh, *Inorg. Chem.*, 2012, **51**, 572; (b) H. J. Choi, M. Dincă, A. Daily and J. R. Long, *Energy Environ. Sci.*, 2010, **3**, 117.
- 17 J. Qian, F. Jiang, D. Yuan, M. Wu, S. Zhang, L. Zhang and M. Hong, *Chem. Commun.*, 2012, **48**, 9696.
- 18 (a) J. Liu, A. I. Benin, A. M. B. Furtado, P. Jakubczak, R. R. Willis and M. D. LeVan, *Langmuir*, 2011, **27**, 11451; (b) A. C. Kizzie, A. G. Wong-Foy and A. J. Matzger, *Langmuir*, 2011, **27**, 6368; (c) H. Jasuja, Y.-g. Huang and K. S. Walton, *Langmuir*, 2012, **28**, 16874; (d) H. Jasuja, J. Zang, D. S. Sholl and K. S. Walton, *J. Phys. Chem. C*, 2012, **116**, 23526; (e) J. B. DeCoste, G. W. Peterson, H. Jasuja, T. G. Glover, Y.-g. Huang and K. S. Walton, *J. Mater. Chem. A*, 2013, **1**, 5642.
- 19 J. Liu, Y. Wang, A. I. Benin, P. Jakubczak, R. R. Willis and M. D. LeVan, *Langmuir*, 2010, **26**, 14301.
- 20 E. Soubeyrand-Lenoir, C. Vagner, J. W. Yoon, P. Bazin, F. Ragon, Y. K. Hwang, C. Serre, J.-S. Chang and P. L. Llewellyn, *J. Am. Chem. Soc.*, 2012, **134**, 10174.
- 21 H. Furukawa, F. Gándara, Y.-B. Zhang, J. Jiang, W. L. Queen, M. R. Hudson and O. M. Yaghi, *J. Am. Chem. Soc.*, 2014, **136**, 4369.
- 22 I. A. Ibarra, S. Yang, X. Lin, A. J. Blake, P. J. Rizkallan, H. Nowell, D. R. Allan, N. R. Champness, P. Hubberstey and M. Schröder, *Chem. Commun.*, 2011, **47**, 8304.
- 23 I. A. Ibarra, K. E. Tan, V. M. Lynch and S. M. Humphrey, *Dalton Trans.*, 2012, **41**, 3920.
- 24 (a) E. Haldoupis, S. Nair and D. S. Sholl, *J. Am. Chem. Soc.*, 2012, **134**, 4313; (b) Y.-S. Bae, O. K. Farha, J. T. Hupp and R. Q. Snurr, *J. Mater. Chem.*, 2009, **19**, 2131.
- 25 I. P. O'koye, M. Benham and K. M. Thomas, *Langmuir*, 1997, **13**, 4054.
- 26 N. L. Ho, F. Porcheron and R. J.-M. Pellenq, *Langmuir*, 2010, **26**, 13287.